

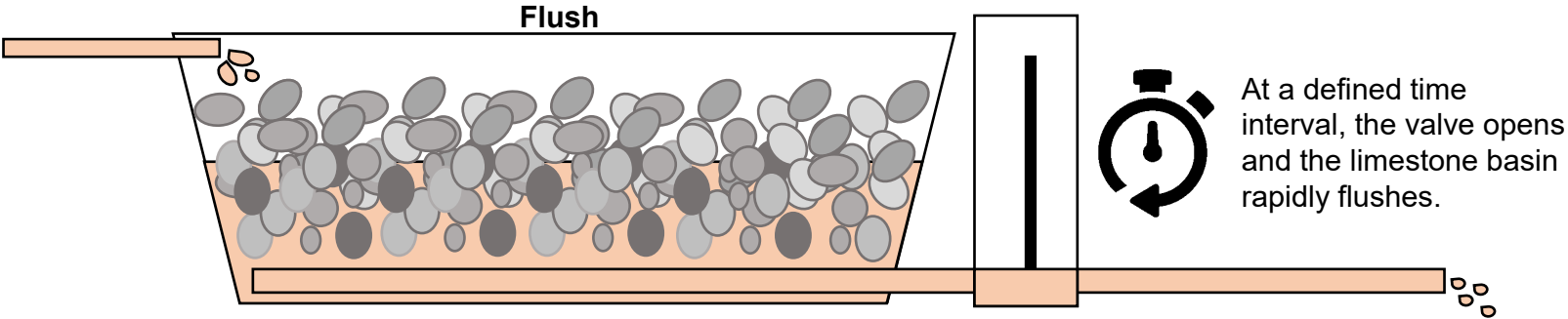
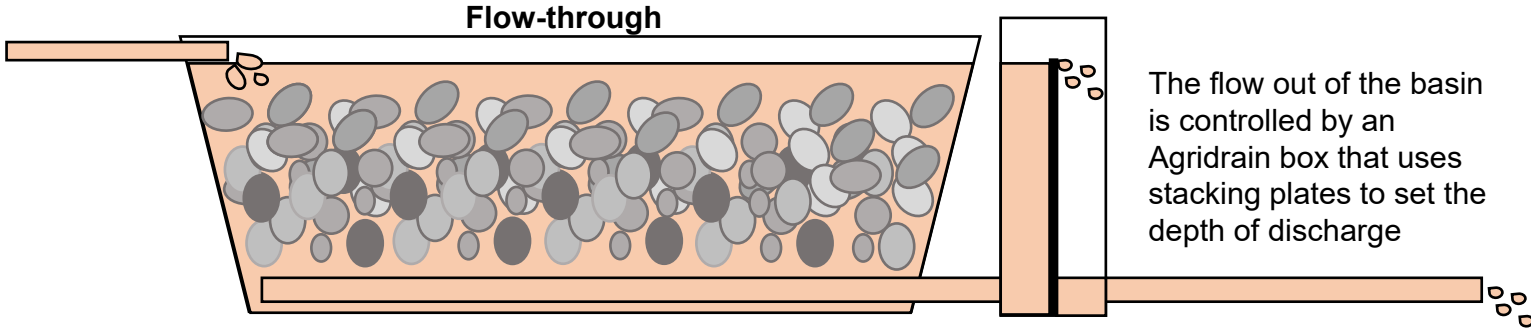
# Batch operating limestone treatment system (BOLTS): a novel approach to treating mine drainage

Tasker, Travis; Roman, Ben; Eckenrode, James; Himes, Nicole; Warner, Henry; Neely, Buck; Denholm, Cliff; Strosnider, William; LaBar, Julie; Danehy, Tim



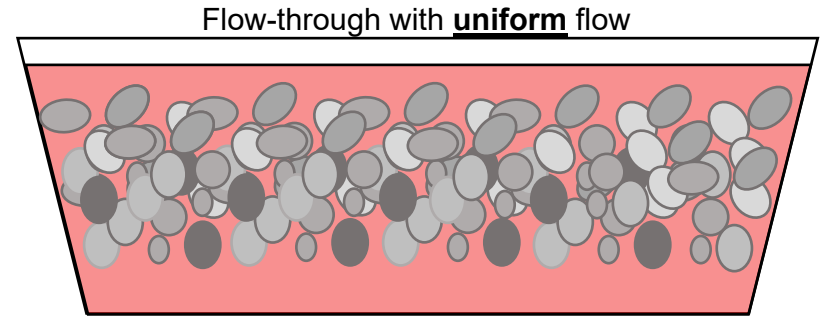
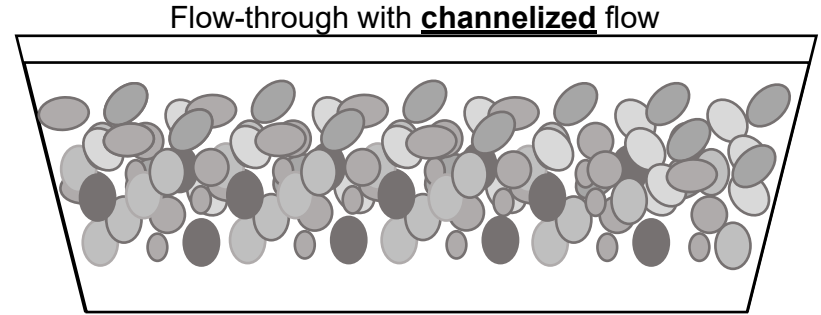
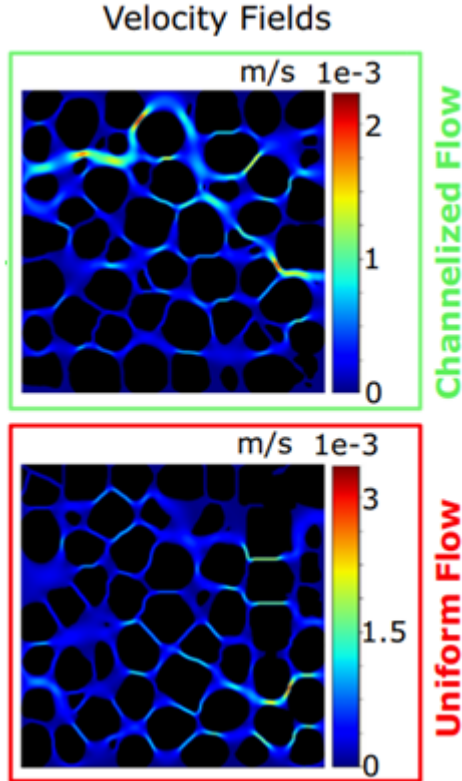
# Typical Auto-Flushing Vertical Flow Pond (AFVFP)

*Continuous flow with periodic flush set by a timer*

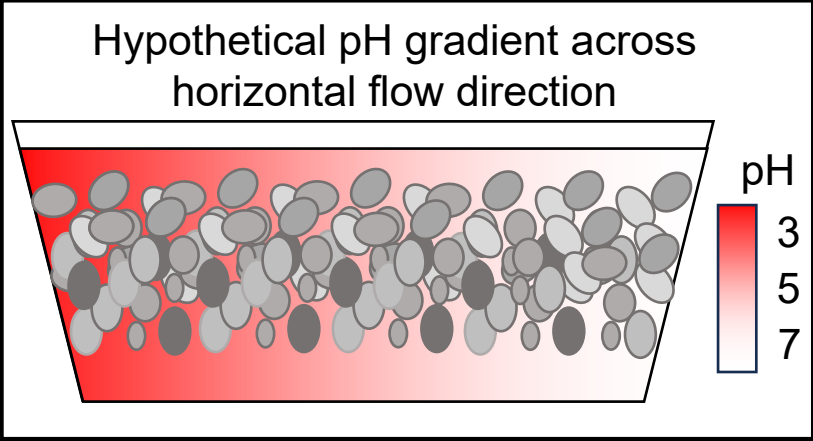




Preferential flow paths occur in heterogenous porous media, likely attributing to a true HRT that is lower than the design HRT.



Flow path also influences HRT and therefore pH → implications for metal precipitation and clogging



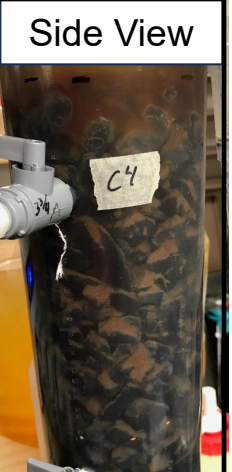
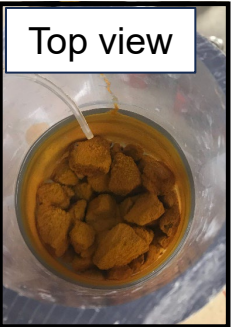
Flow direction

$pH_{in} = 3$   
 $Fe_{in} = 20 \text{ mg/L}$

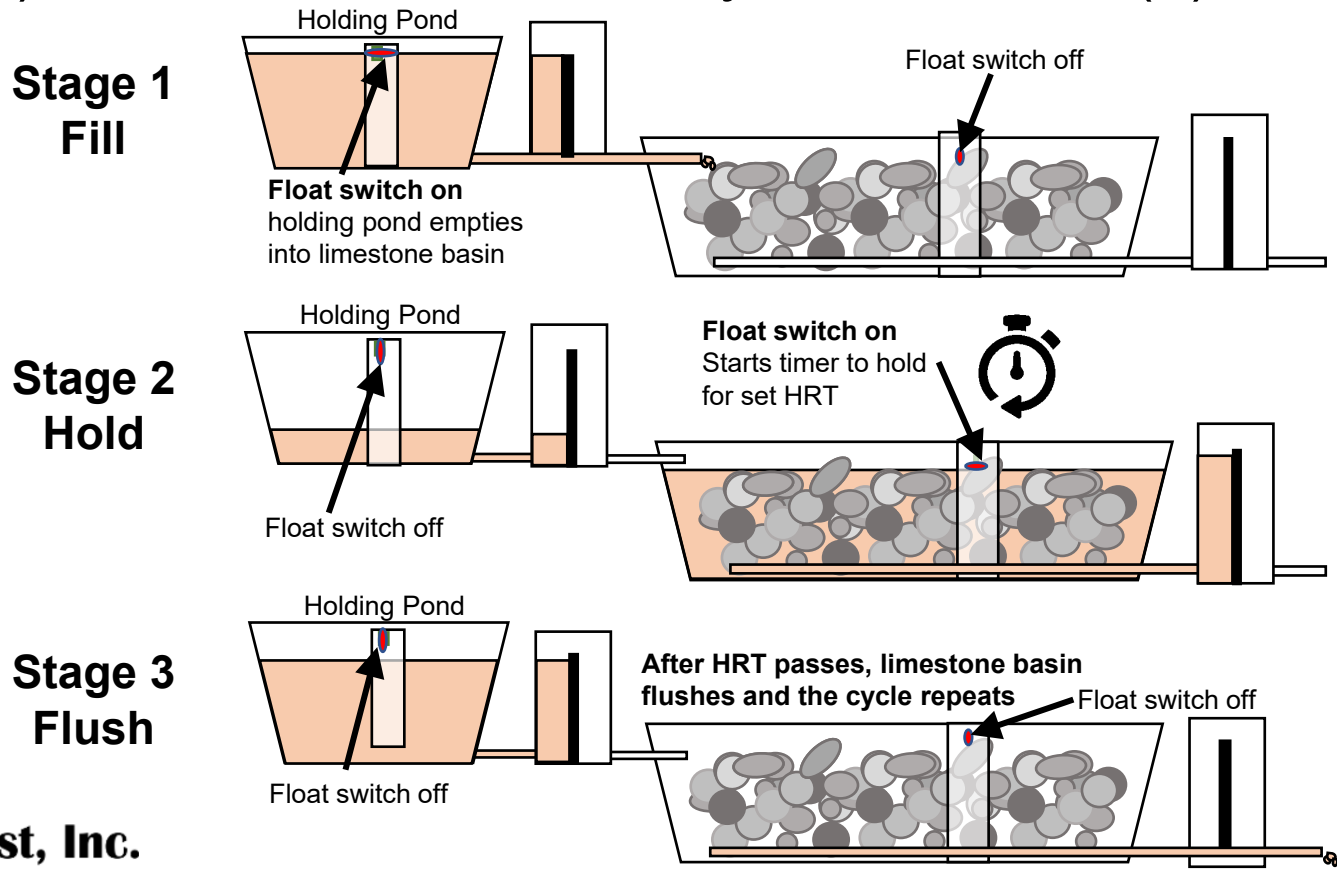
$pH_A = 5.5$   
 $Fe_A = 11 \text{ mg/L}$

$pH_B = 7.4$   
 $Fe_B = 1.5 \text{ mg/L}$

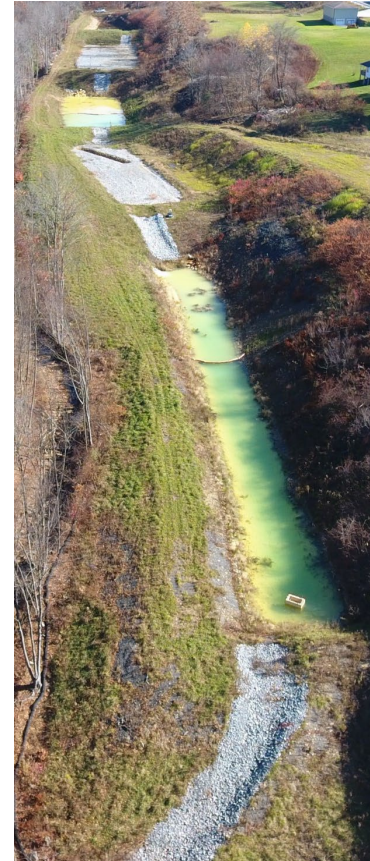
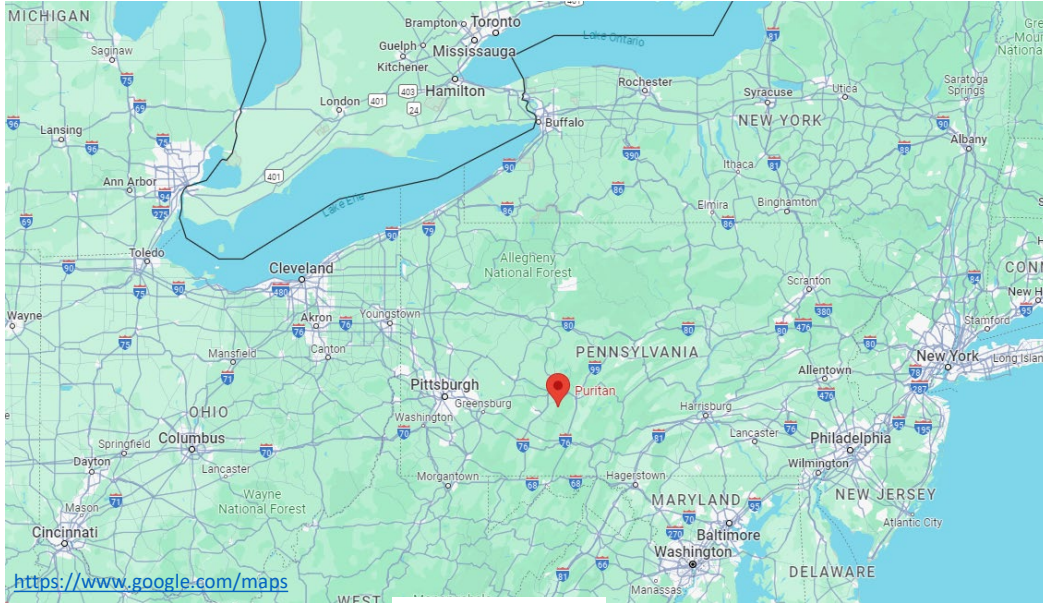
$pH_C = 7.5$   
 $Fe_C < 1 \text{ mg/L}$



# A novel Batch Operating Limestone Treatment System (BOLTS) could increase efficiency of limestone (?)



# A BOLTS was built near Puritan, PA



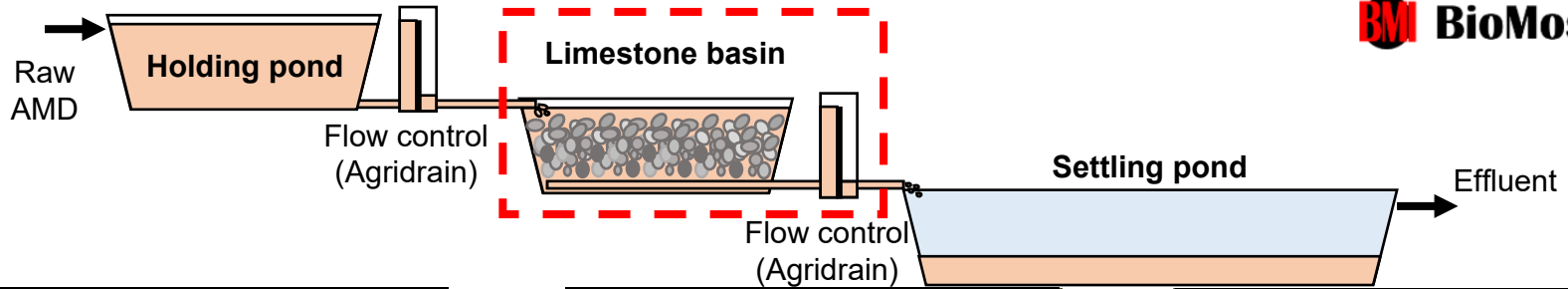
~ 800 feet  
~ 244 meters

Flow (GPM)							
Monitoring Period	n	Minimum	Maximum	Average	Median	95 <sup>th</sup> tile	99 <sup>th</sup> tile
9/1/16 – 8/31/17	30,618	110	1599	261	137	558	664
9/1/17 – 8/31/18	28,886	110	1374	242	209	599	724

Parameter	pH	Conductivity	Acidity	Iron	Manganese	Aluminum	Sulfate
	s.u.	umhos/cm	mg/L	mg/L	mg/L	mg/L	mg/L
Minimum	2.9	1242	77	3.9	1.1	7.7	584
Maximum	3.1	1526	150	9.2	1.6	14.6	709
Average	3.0	1358	114	6.3	1.4	12.0	653
Median	3.1	1328	110	6.0	1.4	12.4	589



The system utilizes a holding pond, solar-powered Agri Drain Smart Drainage water level control structures, and a limestone basin to treat the MD



**Holding pond**



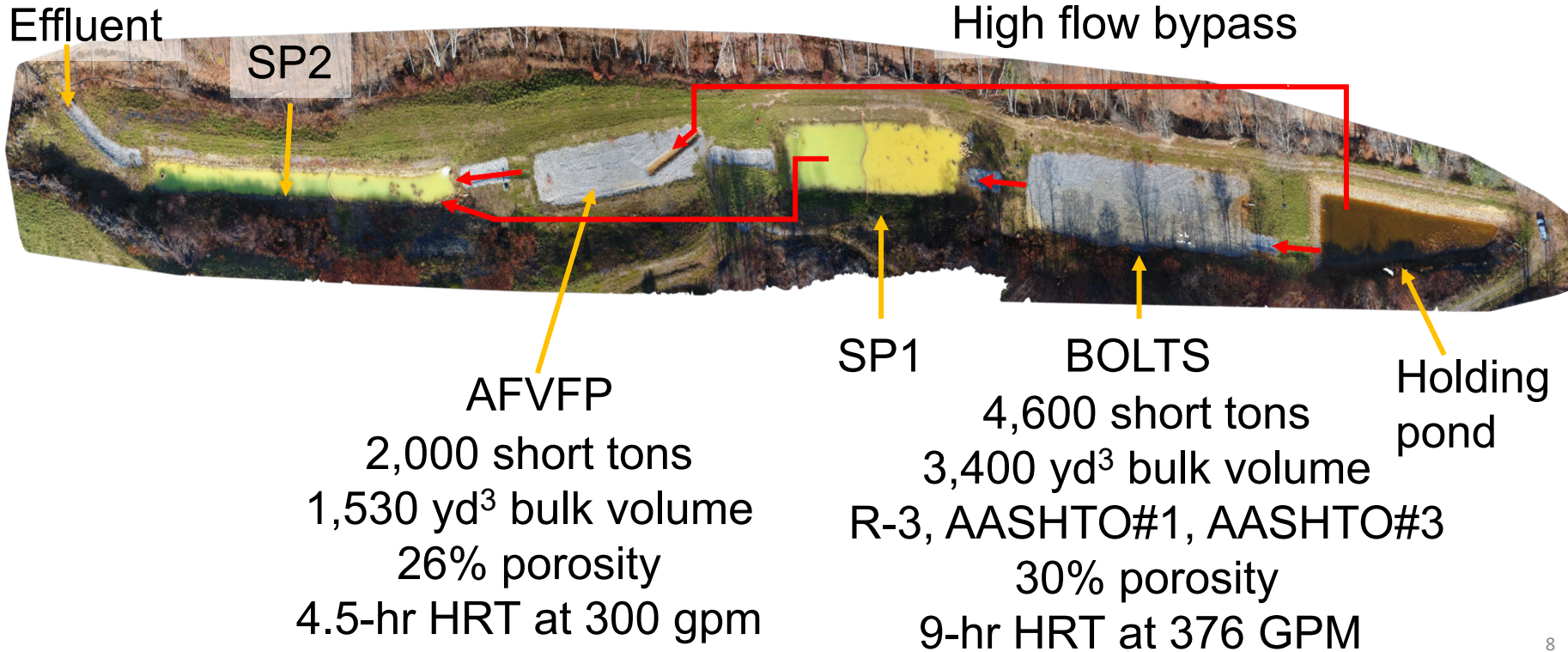
**Limestone basin**



**Settling pond**

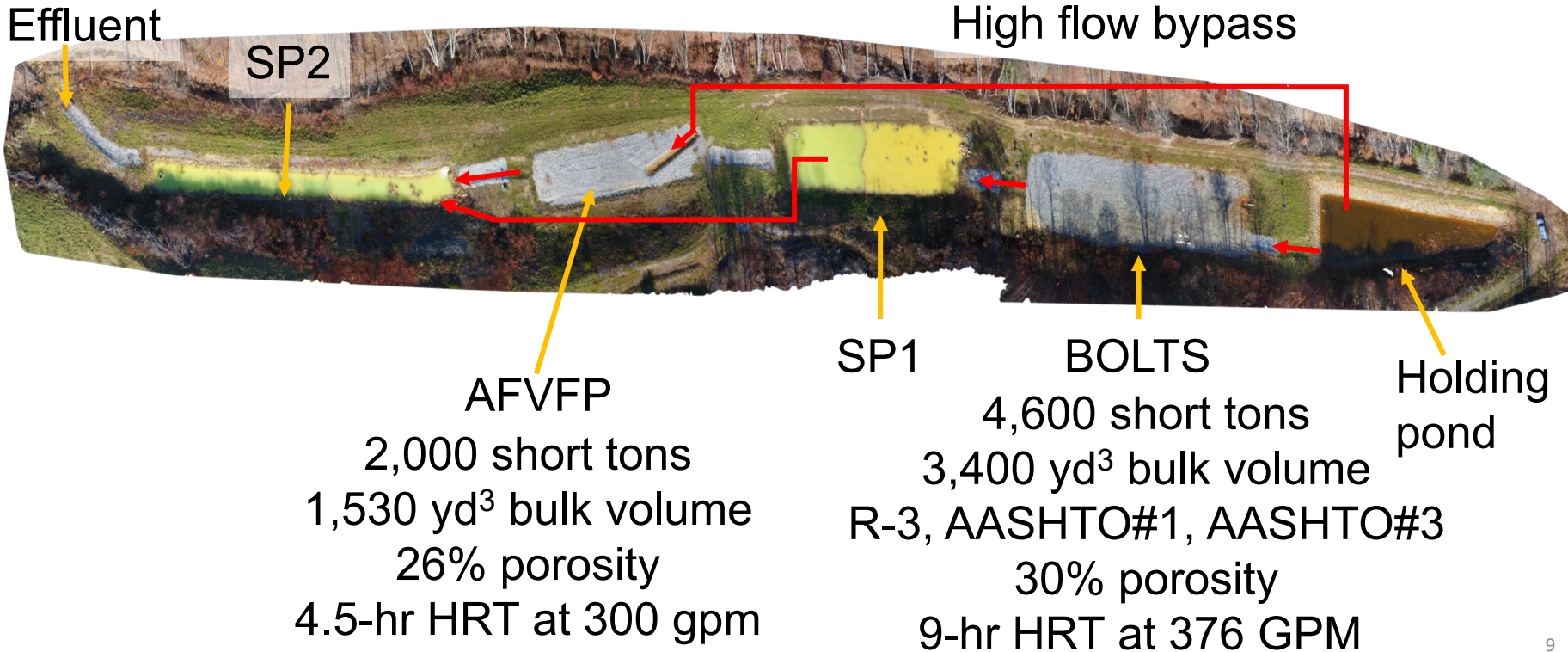


The system utilizes a holding pond, solar-powered Agri Drain Smart Drainage water level control structures, and a limestone basin to treat the MD





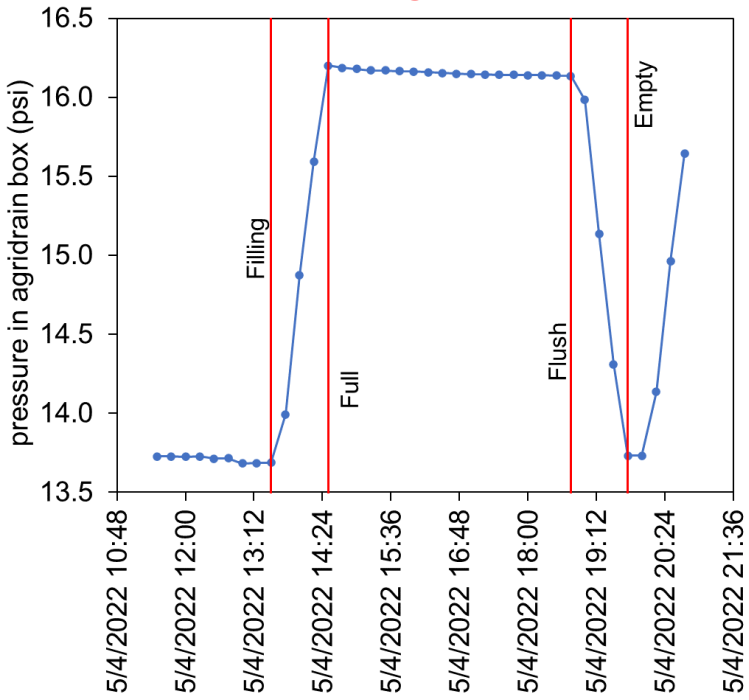
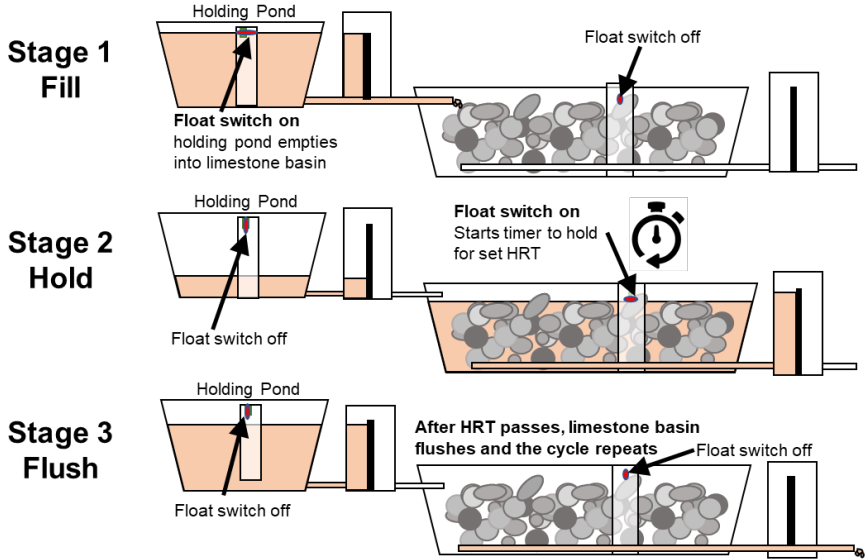
When influent flowrates are > than 282 gpm, the holding pond is full before a 12-hr batch treatment cycle is complete → flow is bypassed into an AFVFP until the batch cycle is complete



In batch treatment mode, the BOLTS can fill and empty within 45 minutes (i.e., 0.75 hours)

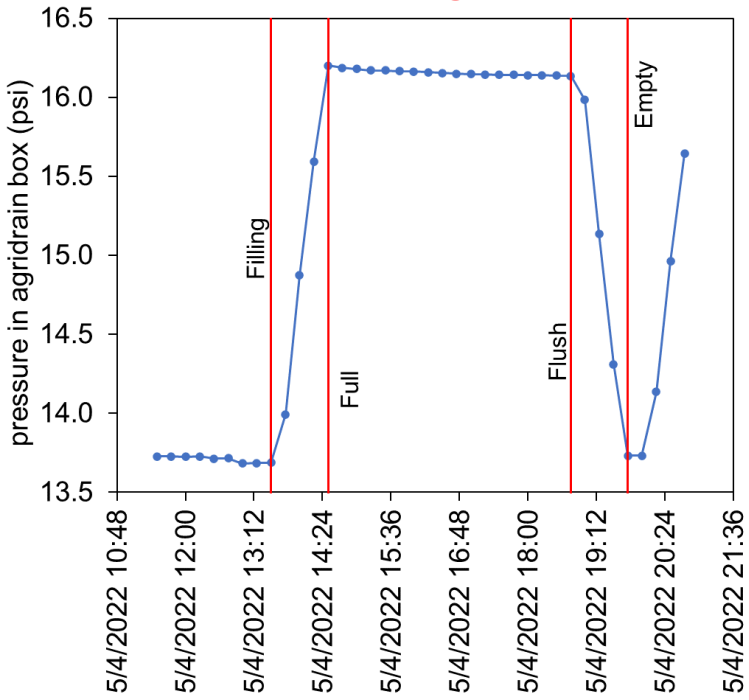
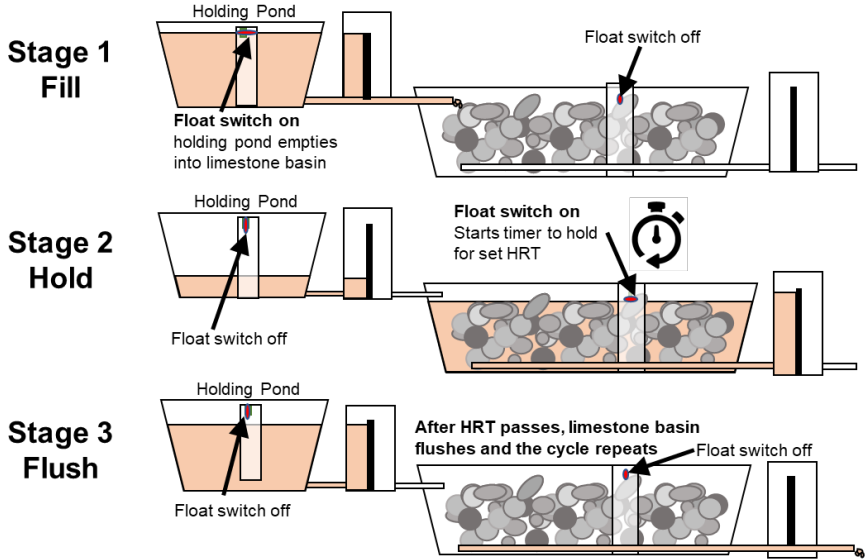
0.75 hours to fill @

? gpm



In batch treatment mode, the BOLTS can fill and empty within 45 minutes (i.e., 0.75 hours)

**0.75 hours to fill @  
(203,040 gal void volume/45 mins) =  
4,512 gpm**

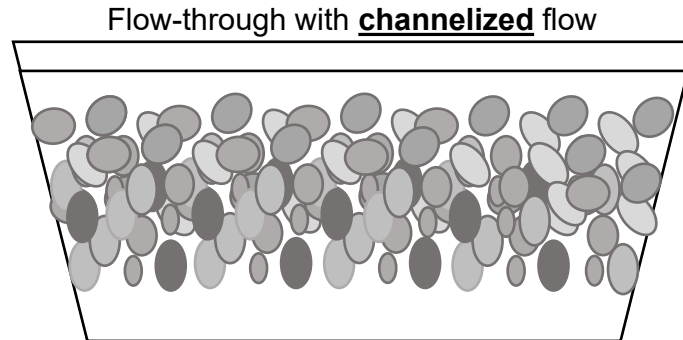




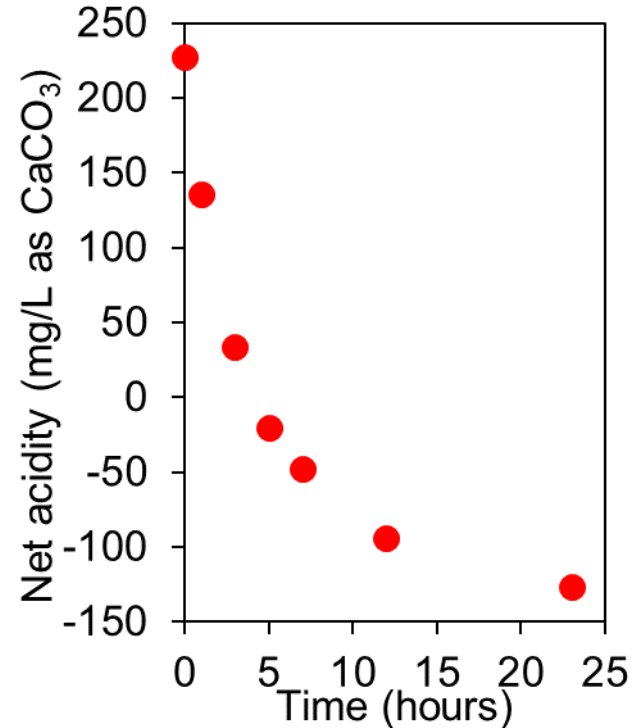


# So. . . . what was the goal of this research?

We hypothesize that a BOLTS overcomes short circuiting and flow challenges that can occur in auto flushing vertical flow pond's (AFVFP's) by allowing “batches” of MD to be treated for a set HRT, producing higher acidity removal rates than a typical horizontal flow AFVFP that operates in flowthrough.

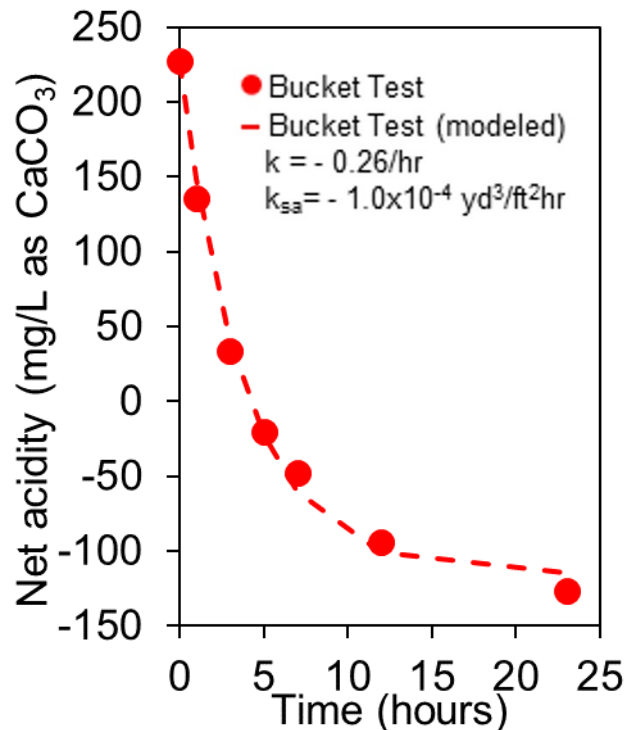


The acidity in the MD from Puritan, PA was neutralized in buckets (full of Puritan limestone) after 5-hour HRT





# A first order model was used to predict net acidity with time elapsed



$$C_t = C_s - [(C_s - C_0) \exp(k t_d)] \quad (\text{Cravotta et al., 2008})$$

$$k_{sa} = k/(A/V)$$

$$A/V = A_u (\rho_b/n)$$

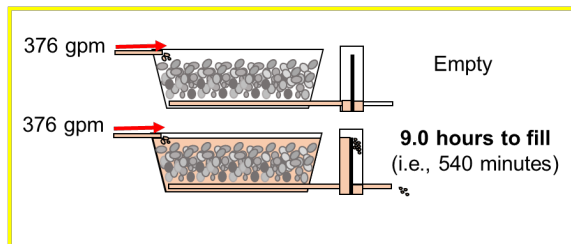
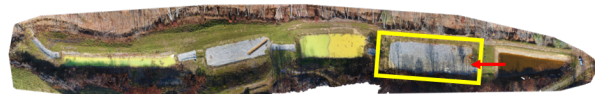
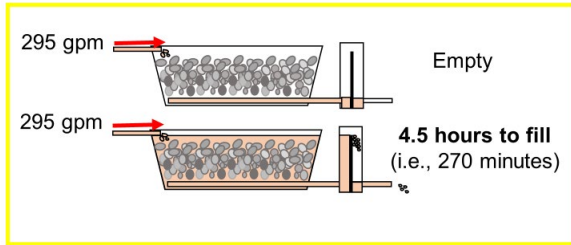
$$A_u = 556 \text{ ft}^2/\text{short ton}$$

$$n = 0.3$$

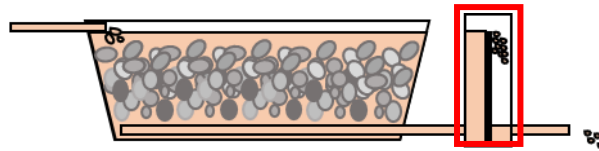
$$\rho_b = 1.35 \text{ short tons}/\text{yd}^3$$

$$A/V = 2500 \text{ ft}^2/\text{yd}^3$$

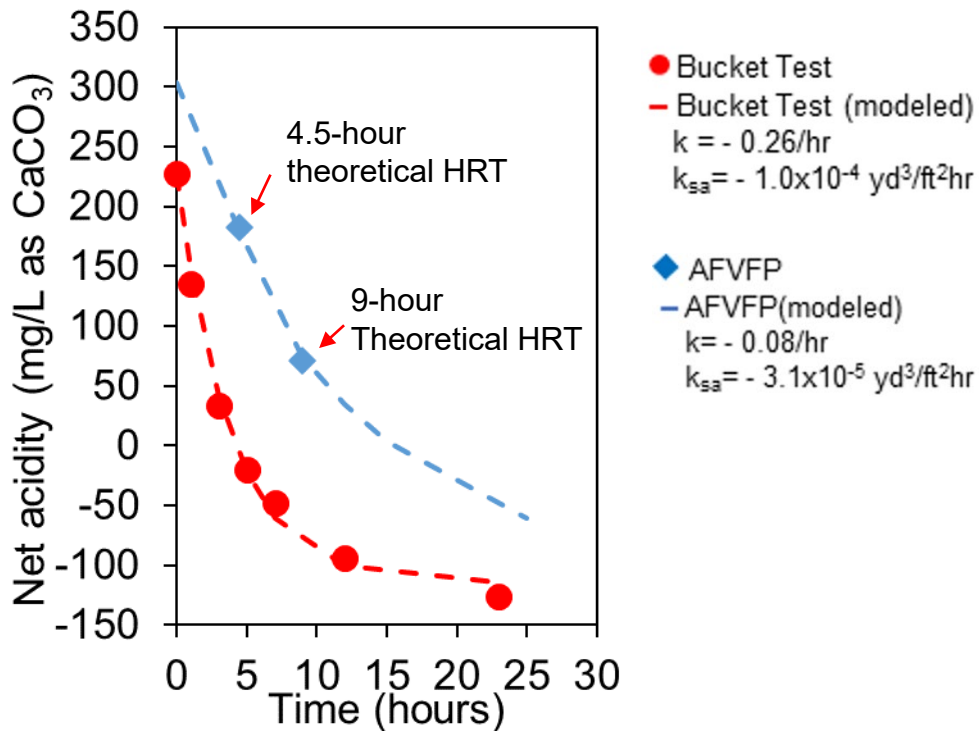
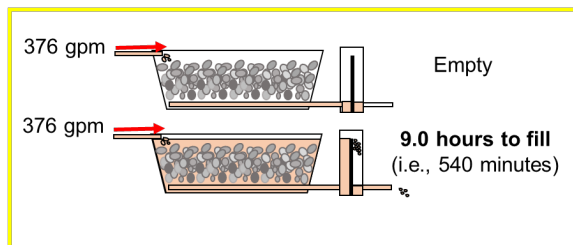
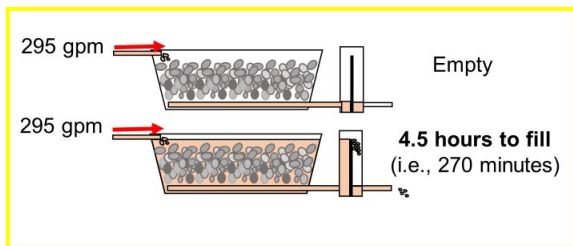
# Acidity was also measured in the effluent of the limestone beds when operated in flowthrough treatment mode



ISCO 3700 water sampler and Eureka Manta+20 water quality monitoring sonde were installed in the Agri Drain box at the outlet of the AFVFP → water samples collected during flow through and flushing



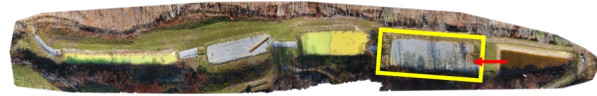
# The AFVFP had a lower acidity removal rate than the bucket tests



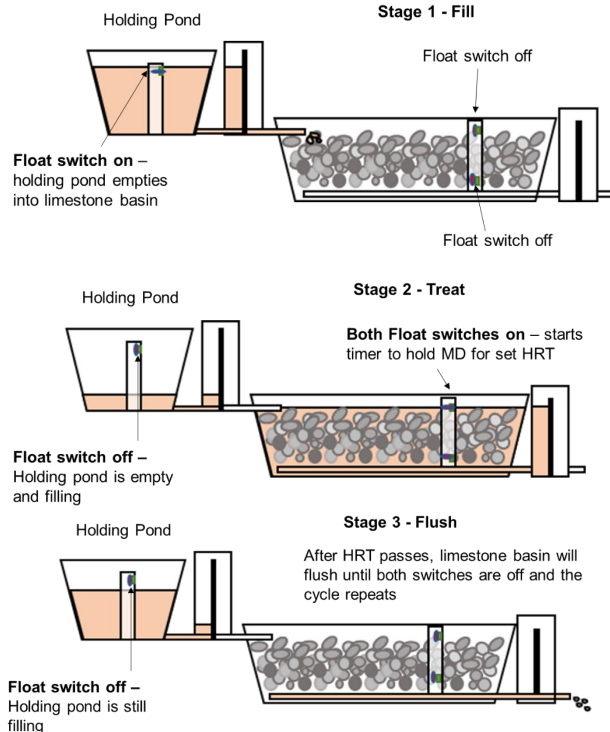


# Acidity was also measured in the effluent of the limestone beds when operated in Batch treatment mode

Treated in batch for 4.5 and 9.0 hours

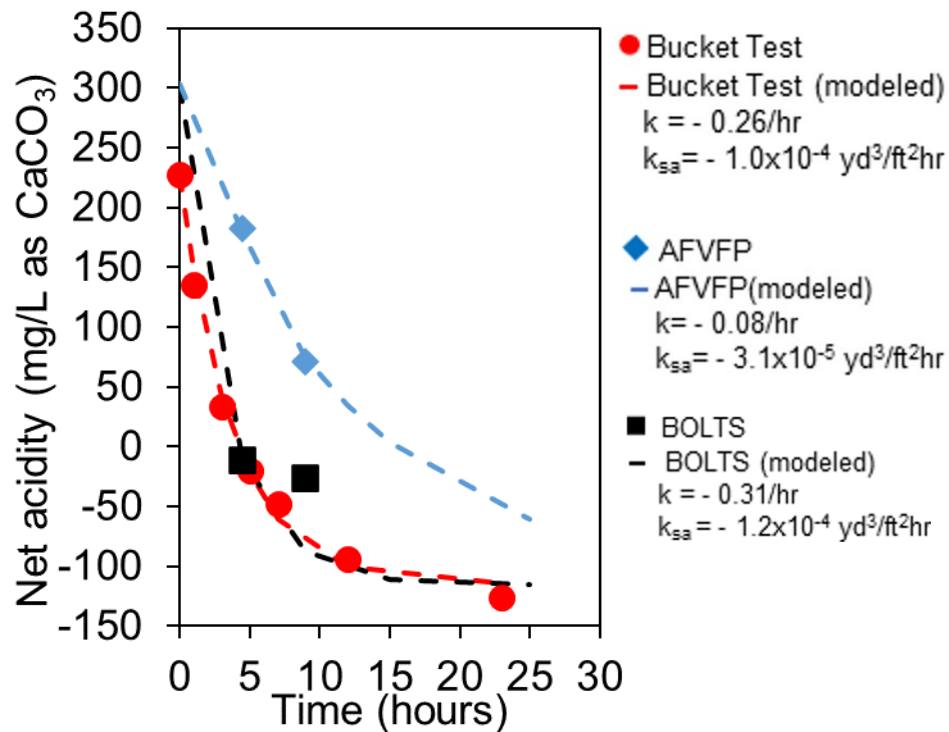
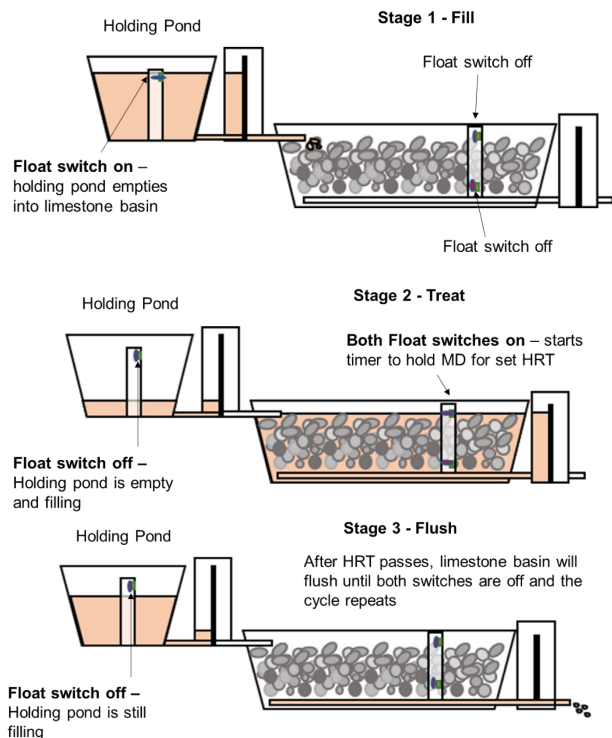


## Measured water chemistry during the 45-minute flush cycle



# The BOLTS had an acidity removal rate that was similar to the bucket tests

Treated in batch for **4.5** and **9.0** hours



# The acidity removal rates were used to compare costs of treating the MD in a BOLTS or AFVFP

$$\text{Mass of limestone} = [(Q C T)/x] + [(Q \rho_b t_d)/(V_v x)] \quad (\text{Hedin and Watzlaf, 1993})$$

Q = flowrate

$\rho_b$  = bulk density of limestone

$t_d$  = detention time (i.e., HRT)

$V_v$  = bulk void volume expressed as a decimal (i.e., the porosity of the stone = n)

C = the predicted concentration of alkalinity or net acidity (i.e.,  $\Delta C$ )

T = design life (i.e.,  $t_L$ )

x =  $\text{CaCO}_3$  content expressed as a percentage



The acidity removal rates were used to compare costs of treating the MD in a BOLTS or AFVFP

$$\text{Mass of limestone} = [(Q C T)/x] + [(Q \rho_b t_d) / (V_v x)] \quad (\text{Hedin and Watzlaf, 1993})$$

Substitute:

$$C_t = C_s - [(C_s - C_0) \exp(k t_d)] \quad \rightarrow \quad t_d = [\ln(C_t - C_s) / C_0 - C_s] / k$$

$$k = k_{sa}(A/V)$$

$$A/V = A_u (\rho_b/n)$$

$$V_v = n$$

$$C = \Delta C$$

$$T = t_L$$

$$\text{Mass of limestone} = M_s = (Q/x)[(t_L \Delta C)] + (Q/x)[\ln[(C_t - C_s)/(C_0 - C_s)] / (k_{sa} A_u)]$$

An AFVFP would require ~2x more limestone than a BOLTS to treat the Puritan MD to -20 mg/L net acidity

Assumptions:

$$Q = 300 \text{ gpm}$$

$$C_o = 250 \text{ mg/L net acidity}$$

$$C_t = -20 \text{ mg/L net acidity}$$

$$C_s = -113 \text{ mg/L net acidity}$$

$$t_L = 20 \text{ years}$$

$$x = 0.9 \text{ (limestone purity)}$$

$$A_u = 556 \text{ ft}^2/\text{short ton (AASHTO\#1 to AASHTO\#3)}$$

$$n = 0.3$$

$$\rho_b = 1.35 \text{ short tons/yd}^3$$

$$k_{sa} = -1.2 \times 10^{-4} \text{ yd}^3/\text{ft}^2\text{hr for BOLTS}$$

$$k_{sa} = -3.1 \times 10^{-5} \text{ yd}^3/\text{ft}^2\text{hr for AFVFP}$$

BOLTS:

$$M_s = (Q/x)[t_L \Delta C] + (Q/x)[\ln[(C_t - C_s)/(C_o - C_s)]/(k_{sa} A_u)]$$

$$M_s = 3952 + 2020 \\ = 5,972 \text{ short tons for BOLTS}$$

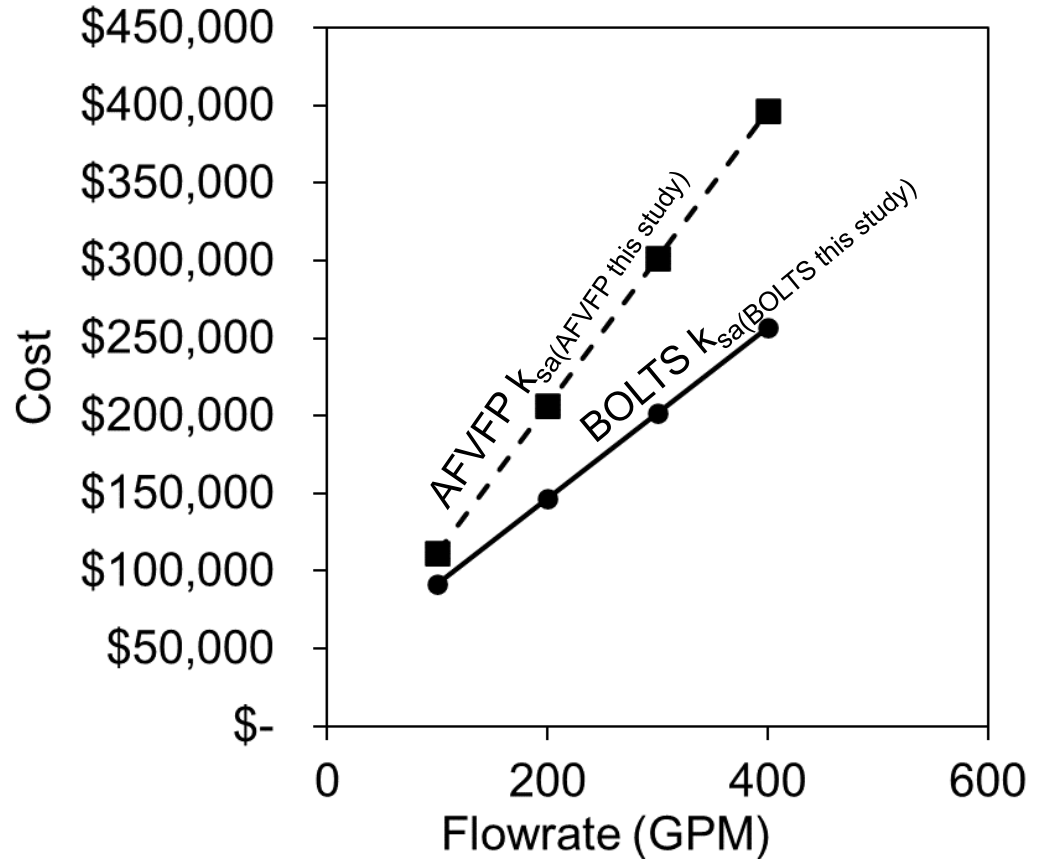
AFVFP:

$$M_s = 3952 + 7822 \text{ short tons} \\ = 11,774 \text{ short tons for AFVFP}$$

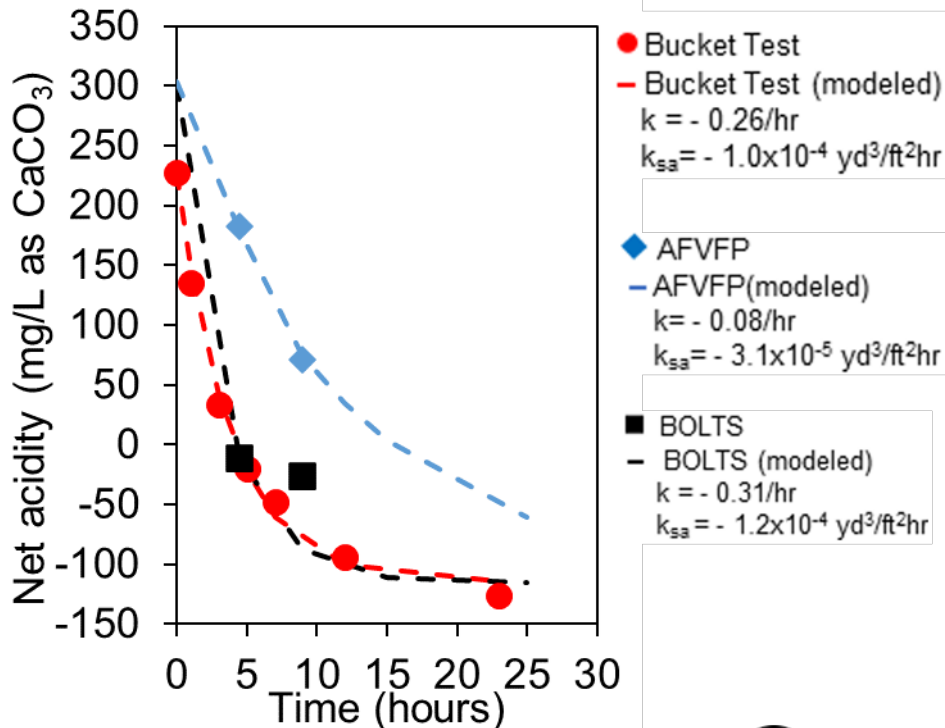
# The BOLTS is cheaper than an AFVFP for treating the Puritan MD

## Assumptions:

- $\rho_b = 1.35$  short tons/ $\text{yd}^3$
- Agri Drain Smart Drain® in BOLTS = \$17,960 per structure
- Agri Drain Smart Drain® in AFVFP = \$15,230 per structure
- \$17.35/short ton of limestone
- \$6.50/ $\text{yd}^3$  of excavation w/ clay liner
- \$13/ft of 12-inch perforated DR-26 HDPE pipe
- \$7.5/ft of 6-inch perforated D pipe
- \$1/ $\text{yd}^2$  of geotextile
- Depth of basins = 8 feet
- Side slopes = 2:1
- Length to width ratio = 5:1



In summary, the BOLTS produced higher acidity removal rates than the AFVFP → new ideas for treating MD?



## Questions?

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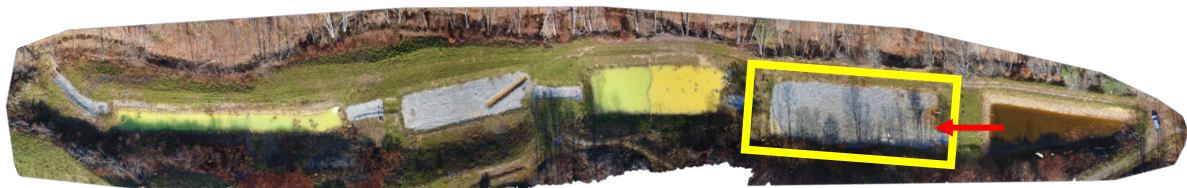




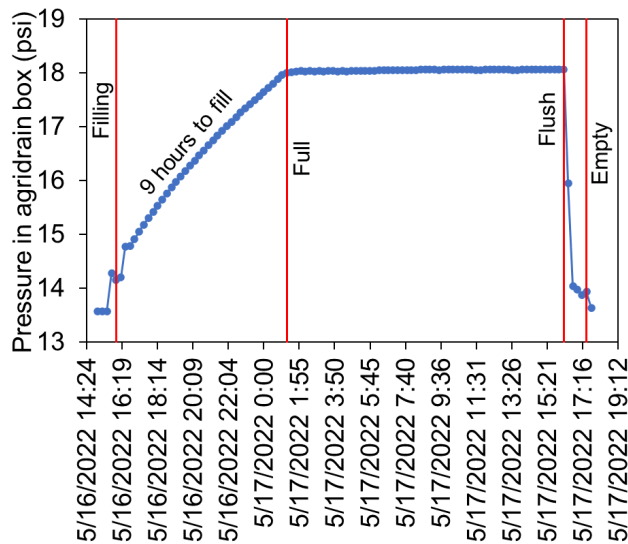
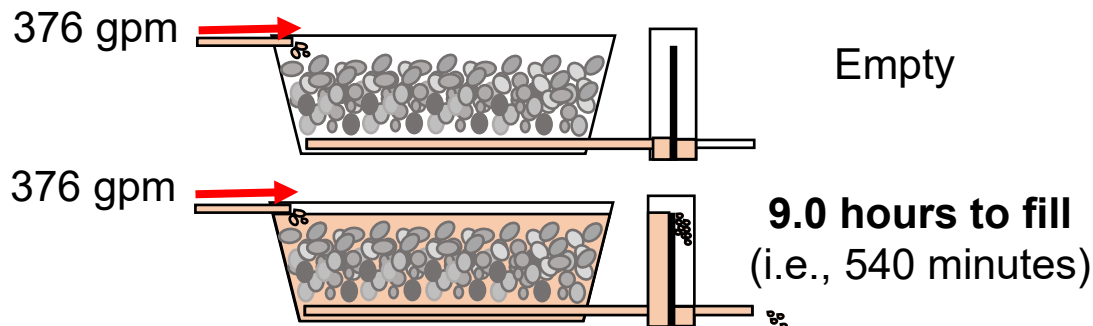
# References

- Cravotta III, C. A. (2008). Laboratory and field evaluation of a flushable oxic limestone drain for treatment of net-acidic drainage from a flooded anthracite mine, Pennsylvania, USA. *Applied Geochemistry*, 23(12), 3404-3422.
- Hedin, R. S., & Watzlaf, G. R. (1993). The effects of anoxic limestone drains on mine water chemistry. Proceedings American Society of Mining and Reclamation. *Proceedings America Society of Mining and Reclamation*, 185 – 194.

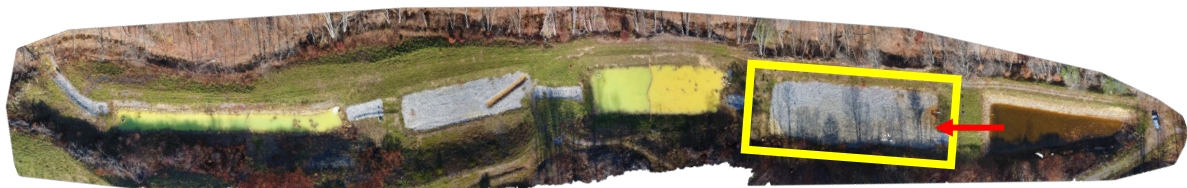
An experiment was performed to see how long it took the BOLTS to fill at continuous influent flow of ~376 gpm



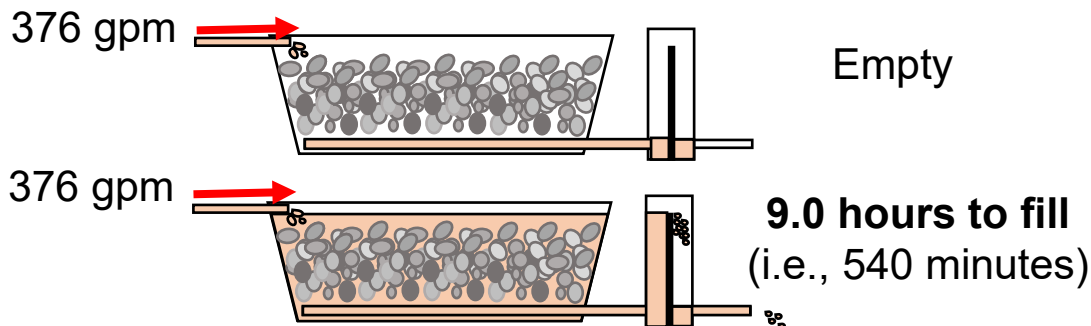
**9 hours to fill @  
376 gpm**



The BOLTS has a bulk volume of 3,400 yd<sup>3</sup>, void volume of 203,040 gallons (i.e., 1005 yd<sup>3</sup>), and porosity of 30%



540 minutes x 376 gal/min  
= **203,040 gallon void volume (i.e., 1005 yd<sup>3</sup>)**



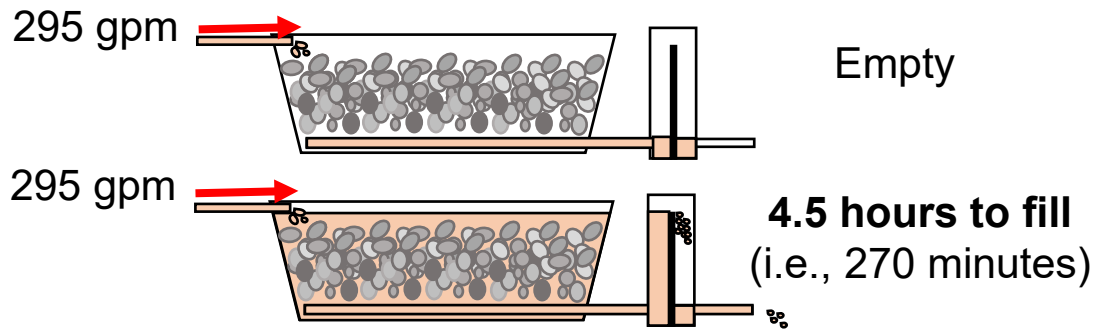
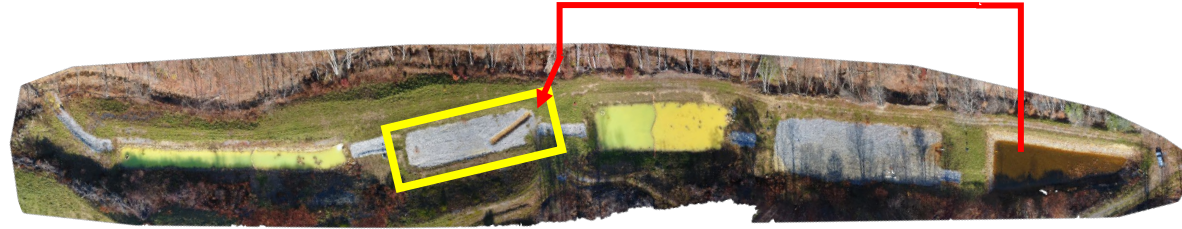
1005 yd<sup>3</sup> void volume /  
3,400 yd<sup>3</sup> bulk volume  
= **30% porosity**

Bulk density = 4,600 short tons /  
3,400 yd<sup>3</sup> bulk volume  
= **1.35 short tons / yd<sup>3</sup>**





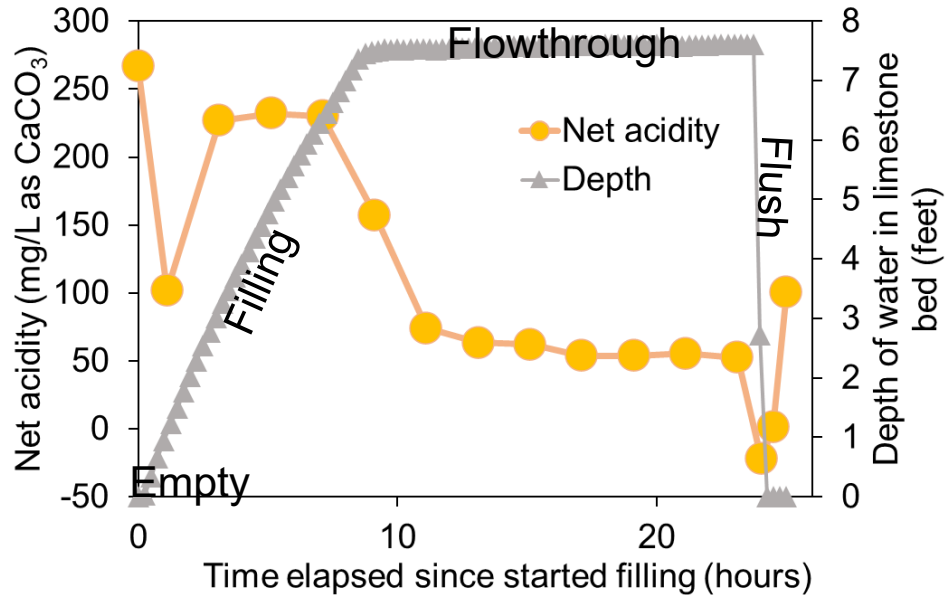
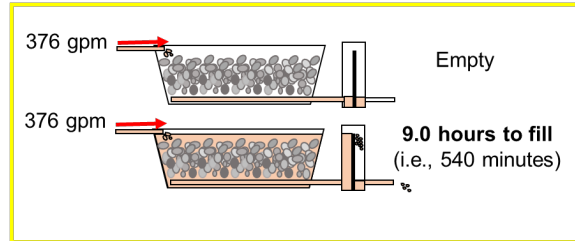
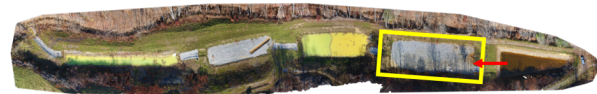
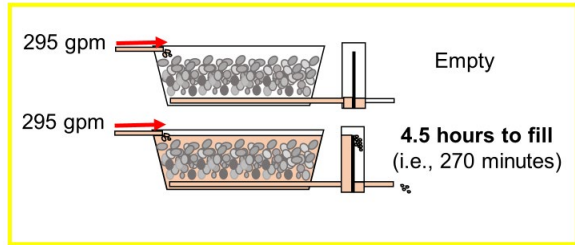
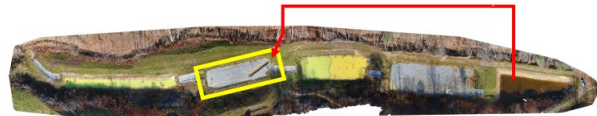
The AFVFP has a bulk volume of 1,530 yd<sup>3</sup>, void volume of 79,650 gallons (i.e., 394 yd<sup>3</sup>), and porosity of 26%



270 minutes x 295 gal/min  
= **79,650 gallon void  
volume (i.e., 394 yd<sup>3</sup>)**

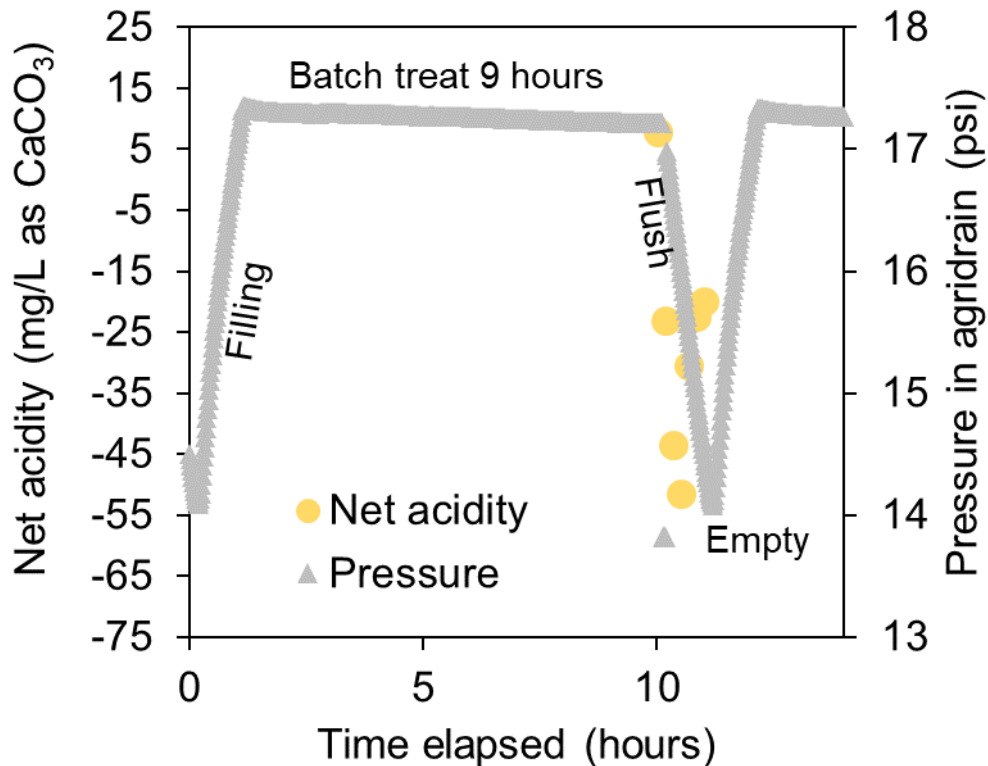
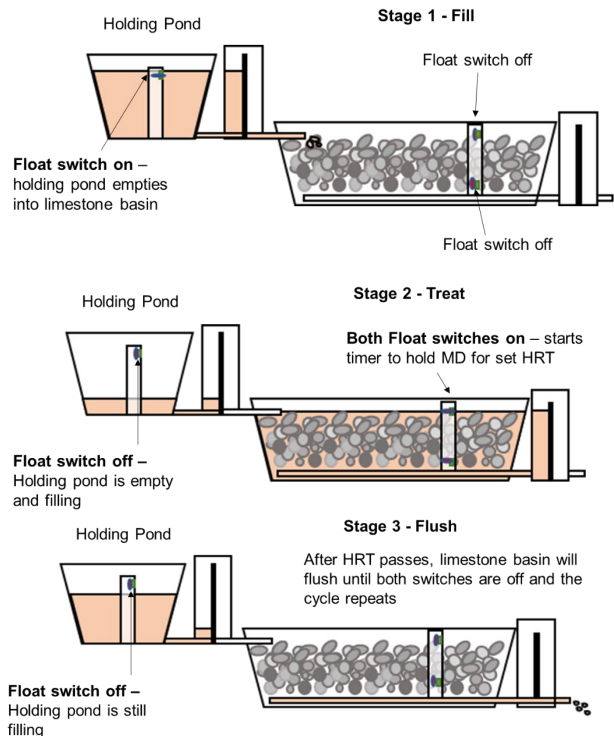
394 yd<sup>3</sup> void volume /  
1,530 yd<sup>3</sup> bulk volume =  
**26% porosity**

# Average net acidity in the effluent during flowthrough treatment mode (9-hour theoretical HRT) was 71 mg/L



BOLTS with 9 hour hold time → the average net acidity during the flush was -26 mg/L

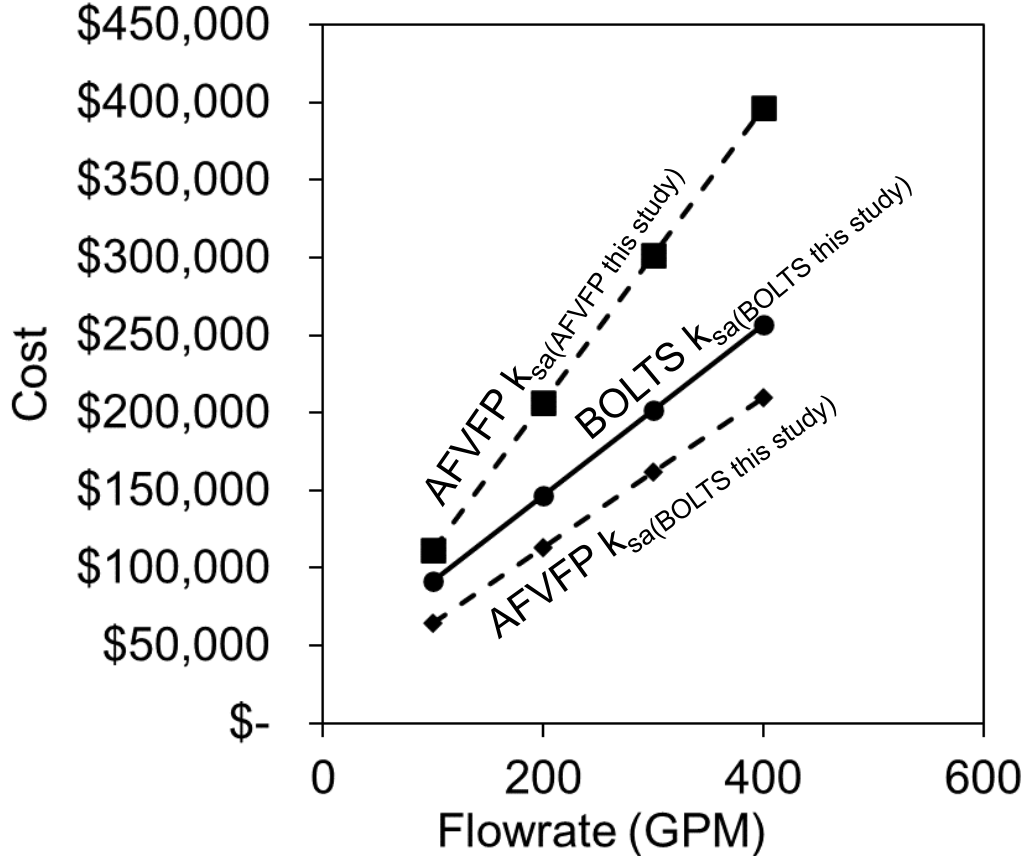
Treated in batch for 4.5 and 9.0 hours



# AFVFP would be cheaper than the BOLTS if sized with same $k_{sa}$ as BOLTS

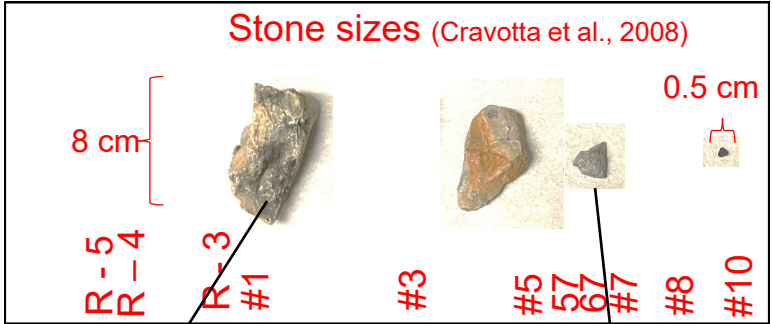
Assumptions:

- $\rho_b = 1.35$  short tons/yd<sup>3</sup>
- Agri Drain Smart Drain® in BOLTS = \$17,960 per structure
- Agri Drain Smart Drain® in AFVFP = \$15,230 per structure
- \$17.35/short ton of limestone
- \$6.50/yd<sup>3</sup> of excavation w/ clay liner
- \$13/ft of 12-inch perforated DR-26 HDPE pipe
- \$7.5/ft of 6-inch perforated D pipe
- \$1/yd<sup>2</sup> of geotextile
- Depth of basins = 8 feet
- Side slopes = 2:1
- Length to width ratio = 5:1





# Could the MD be treated faster with smaller stone size?



$$C_t = C_s - [(C_s - C_0) \exp(k t_d)]$$

$$k_{sa} = k/(A/V)$$

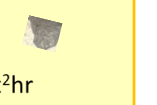
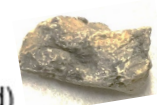
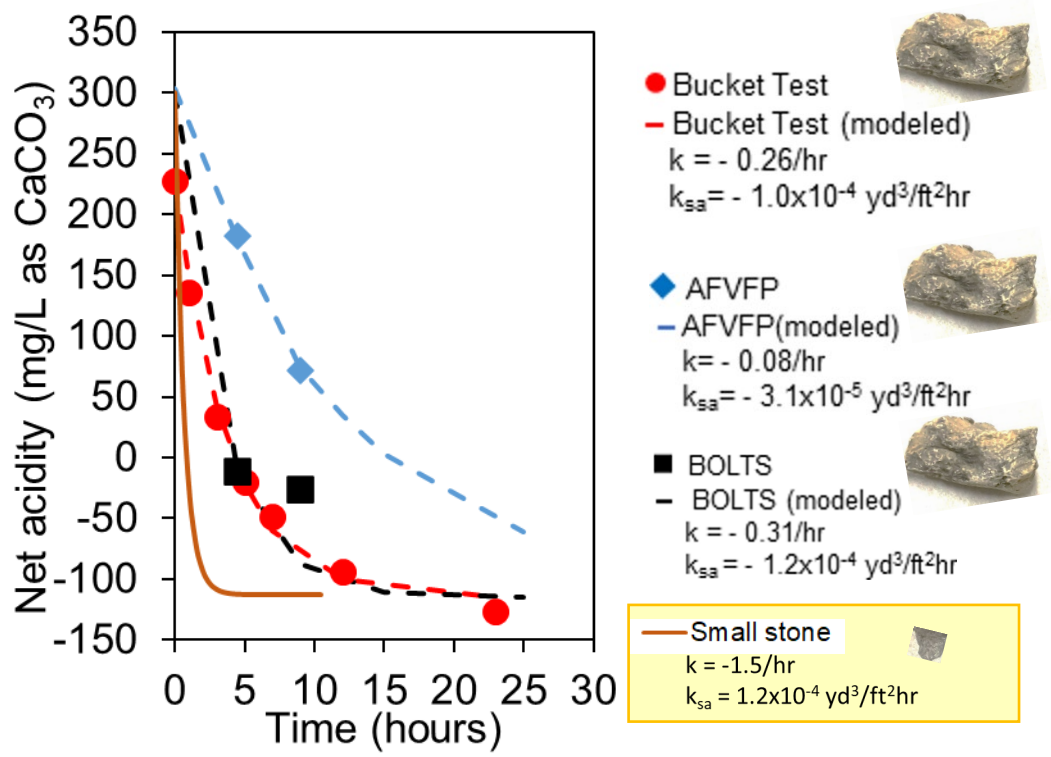
$$A/V = A_u (\rho_b/n)$$

$$k = k_{sa}[A_u (\rho_b/n)]$$

$A_u = 556 \text{ ft}^2/\text{short ton}$   
for AASHTO#1 /  
AASHTO#3

$A_u = 2,800 \text{ ft}^2/\text{short ton}$   
for AASHTO#7

# If stone size was reduced, the MD could be treated faster



# If stone size was reduced, would require 27% less limestone to treat the MD

## Assumptions:

$$Q = 300 \text{ gpm}$$

$$C_o = 250 \text{ mg/L net acidity}$$

$$C_t = -20 \text{ mg/L net acidity}$$

$$C_s = -113 \text{ mg/L net acidity}$$

$$t_L = 20 \text{ years}$$

$$x = 0.9 \text{ (limestone purity)}$$

$$A_u = 556 \text{ ft}^2/\text{short ton (AASHTO\#1 to AASHTO\#3)}$$

$$A_u = 2,800 \text{ ft}^2/\text{short ton (AASHTO\#7)}$$

$$n = 0.3$$

$$\rho_b = 1.35 \text{ short tons/yd}^3$$

$$k_{sa} = -1.2 \times 10^{-4} \text{ yd}^3/\text{ft}^2\text{hr for BOLTS}$$

$$k_{sa} = -3.1 \times 10^{-5} \text{ yd}^3/\text{ft}^2\text{hr for AFVFP}$$



$$M_s = (Q/x)[t_L \Delta C] + (Q/x)[\ln[(C_t - C_s)/(C_o - C_s)]/(k_{sa} A_u)]$$

$$k_{sa} = -1.2 \times 10^{-4} \text{ yd}^3/\text{ft}^2\text{hr for BOLTS}$$

$$A_u = \underline{556 \text{ ft}^2/\text{short ton}} \text{ for AASHTO\#1 to \#3}$$

$$M_s = \underline{5,972 \text{ short tons}} \text{ for AASHTO\#1 / AASHTO\#3}$$

$$A_u = \underline{2,800 \text{ ft}^2/\text{short ton}} \text{ for AASHTO\#7}$$

$$M_s = \underline{4,340 \text{ short tons}} \text{ for AASHTO\#7}$$

# Cost of BOLTS would decrease from \$200,000 to \$150,000 if used smaller stone size

Assumptions:

- $\rho_b = 1.35$  short tons/yd<sup>3</sup>
- Agri Drain Smart Drain® in BOLTS = \$17,960 per structure
- Agri Drain Smart Drain® in AFVFP = \$15,230 per structure
- \$17.35/short ton of limestone
- \$6.50/yd<sup>3</sup> of excavation w/ clay liner
- \$13/ft of 12-inch perforated DR-26 HDPE pipe
- \$7.5/ft of 6-inch perforated D pipe
- \$1/yd<sup>2</sup> of geotextile
- Depth of basins = 8 feet
- Side slopes = 2:1
- Length to width ratio = 5:1

