

# Performance of natural and residual materials for mine water treatment and mine sites rehabilitation

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# **Research topics**



#### **Industrial partners mine sites**



https://www.uqat.ca/uqat/departements/irme/



## Introduction: Mines and water contamination

|                       | Mine drainage (runoff water)  |                                | N-based compounds (mine effluents)         |                              |
|-----------------------|---|--------------------------------|--|------------------------------|
| Contaminants          | AMD<br>(acid mine drainage)   | NMD<br>(neutral mine drainage) | CN⁻, SCN⁻                                  | Ammonia (NH <sub>3</sub> -N) |
| Sources               | Metal sulfides + O <sub>2</sub> + water   |                                | Au, Ag extraction + blasting agents (ANFO) |                              |
| Characteristics       | pH < 3; high [] metals<br>(Fe >1g/L), sulfates  | Metal [] > criteria            | Ore dependent, <b>but [] &gt; criteria</b> |                              |
| Why prevent or treat? | Regulation, environmental and social impacts  |                                |  |                              |
| Challenges            | Several contaminants  | High contaminant mobility      | Complexity (toxicity, costs, flowrates)    |                              |
| Treatment issues      | Sludge management<br>(quantity, stability)  | Limited knowledge              | Low kinetics of N oxidation                |                              |
| Research work (RIME)  | Use of natural and residual materials (raw vs modified) for prevention and control of mine water contamination, and mine sites rehabilitation |                                |  |                              |



#### Natural and residual materials for mine water treatment and sites rehabilitation

| Case study                   | AMD/NMD prevention                                       | Passive treatment  |
|------------------------------|--|--|
| I: East-Sullivan mine site   | Residual organics cover                                  | Constructed wetlands + water pumping through the organic cover |
| II: Manitou mine site        | Desulfurized non-acid generating tailings cover          | (To be designed and constructed)                               |
| III: Wood-Cadillac mine site | Inert sand-based cover                                   | Wood-based biofilter   |
| IV: Lorraine mine site       | CCBE (cover with capillary barrier effect) – multi-layer | Anoxic dolomite drains + tri-unit biochemical train            |

| V: New materials  | Modification / Improvement                           | Use                                       |  |
|-------------------|--|---|--|
| Charred dolomite  | Enhanced specific surface and porosity, increased pH | Synthetic NMD treatment                   |  |
| Modified wood ash | and alkalinity generation                            | Real NMD treatment                        |  |
| Activated biochar | Porosity arrangement                                 | Real AMD treatment                        |  |
| N-rich residuals  | N/A  | Non-acid generating tailings revegetation |  |

- Ongoing research
- Concluding remarks



### Location of East-Sullivan and Manitou mine sites



#### East-Sullivan mine site: operation, abandonment, rehabilitation



(http://sebastienlavoie.com/maitrise/photos.html; http://www.mrn.gouv.qc.ca/mines/restauration/restauration-sites-east-sullivan.jsp; https://www.oiseauxduquebec.org)



#### East-Sullivan organic cover: mine site rehabilitation

- 1984: Organic waste (residual wood and biosolids) cover instalment for AMD prevention and [temporary] treatment
- **1990:** Seepage collection system
- 1992-1996: Confining dike (6 km) + water polishing in constructed wetlands
- 1998-2005: Collected AMD in constructed wetlands pumping through the organic cover
- $\circ$  **2019-2020:** Wood cover completion
  - $\Rightarrow$  Some effluents were still acidic



Figure 1. Map of the East Sullivan tailings impoundment in 1994





### East-Sullivan organic cover: mine site monitoring

- Network of sampling points
  - over 20-year data
- Parameters analyzed
  - pH, Fe, Cu, Zn (+ Al, Mn, Pb, SO<sub>4</sub><sup>2-</sup>)
- Compliance, except for the last covered tailings















• Covered tailings and constructed wetlands: **blooming vegetation** and **birds' refugee** (> 190 species listed)

(Rakotonimaro et al., 2015; Malki & Roy, 2024; https://www.google.ca/flickr.com)



### Desulfurized tailings cover: Manitou mine

II

Prevention and pretreatment of AMD (pH: 2-3; 10-12 g/L Fe; 0.6-1 g/L Zn; 0.1-1 g/L Cu; 30-40 g/L SO<sub>4</sub><sup>2-</sup>)



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### Sand cover + wood-based biofilter: Wood-Cadillac mine site

Efficient passive treatment of As-NMD: removal of As & metals; decrease of SO<sub>4</sub><sup>2-</sup> [] to < 200 mg/L</li>



(Germain & Cyr, 2003; Libéro, 2007; Mehdaoui et al., 2024; Thevenot et al., 2024) 11



### CCBE + passive treatment: Lorraine mine site



outlet





- 1964-1968: Extraction of Cu, Au, Ag, and Ni 0
  - Acid generating tailings: 15.5 ha (up to 6 m)  $\succ$
  - AMD: pH=3.6, 7 g/L Fe and 15 g/L sulfates  $\succ$
- In 1998: Mine site reclamation 0
  - Multi-layer dry cover with capillary barrier effect (**CCBE**): O<sub>2</sub> prevention  $\geq$
  - AMD treatment: 3 anoxic dolomite drains (Dol-1 to Dol-3)

- In 2011: Dol-3 clogged, replaced by tri-unit system: PBR1-WA-PBR2 0 (AMD: pH < 4, 3g/L Fe)
  - PBR1: 40% organics, 60% inorganics (pH /, sulfate removal)  $\geq$
  - WA: 100 % wood ash (Fe treatment)  $\triangleright$
  - PBR2: 77% organics, 23 % inorganics (polishing)



(Jouini et al., 2022)

#### • Tri-unit system progressive loss of efficiency: PBR1-WA-PBR2

> **Porosity clogging** by Fe minerals

 $\triangleright$ 

 $\geq$ 

 $\geq$ 

10" 10"

> Preferential flow and partial water bypassing the system



FM (x2)

20000

16000

12000

2000

13





1 polishing unit (50% calcite + 50% wood chips)

2 Fe pretreatment units (50% wood chips + 50% wood ash)





LM-2

LM-1

LM-3

10000

8000

(J/gm)

S042



#### New materials: Sources and modification procedures



|                       | Parameter           |          | Composition (%)                                    |                                 |                   |
|-----------------------|---------------------|----------|--|---------------------------------|-------------------|
| Material              | pH <sub>paste</sub> | Porosity | Dolomite<br>[CaMg(CO <sub>3</sub> ) <sub>2</sub> ] | Calcite<br>[CaCO <sub>3</sub> ] | Magnesia<br>[MgO] |
| Raw dolomite          | 7.9                 | 0.44     | 87.1   | BDL                             | BDL               |
| Half-charred dolomite | 11.6                | 0.56     | 7.2  | 53.7                            | 19.9              |

• Half-charred dolomite: dolomite content decreased, two new minerals were created



| Parameter           | Ash B | Ash B modified | Ash W | Ash W modified |
|---------------------|-------|----------------|-------|----------------|
| pH <sub>paste</sub> | 13.8  | 12.6           | 9.3   | 12.8           |
| CEC, meq /100g dry  | 138   | 322            | 66    | 311            |

• Wood ash: modification generated high CEC and paste pH new materials





**Step 2:** Activation (chemically: KOH,  $H_3PO_4$  or physically: steam,  $CO_2$ )



Activated biochar: arranged porosity

Step 1: Torrefaction, slow to flash pyrolysis, or gasification under different operating conditions

(Calugaru et al., 2016-2020; Braghiroli et al., 2018)



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### Raw vs modified dolomite: Ni, Zn removal in synthetic NMD

#### • Significantly better efficiency of charred dolomite for Ni and Zn removal (50 mg/L each)



Va

### Raw vs modified wood ash: Ni, Zn removal in real NMD



Effluent #1 (pH 7.89, 3.71 mg/L Ni)

Ni removal (<0.5 mg/L)</li>

2h for both modified ash (MAB & MAW)

- Effluent #2 (pH 6.85, 9.1 mg/L Zn)
  - Zn removal (<0.5 mg/L)</li>
    - $\circ$  2h for MAB
    - 7 days for MAW (93% within 2h), but 2h for Mn removal (99% of 4.2 mg/L)



(Calugaru et al., 2017)

### Activated biochar: Cu removal in real AMD

• KOHBBS: Efficient for Cu removal in real effluents

S<sub>BET</sub> = 1700 m<sup>2</sup>/g; 100% de micropores; 22.4% oxygenated groups



| Parameter | Real AMD<br>(mg/L) | After adsorption<br>(KOHBBS)<br>(mg/L) | Efficiency<br>(%) |
|-----------|--------------------|--|-------------------|
| Со        | 9.4                | 0.5                                    | 95 🗸              |
| Cu        | 1.75               | 0.006                                  | ~ 100 🗸           |
| Fe        | 468                | 405                                    | 13 🗸              |
| Mn        | 10.9               | 9.7                                    | 11 ↓              |
| Pb        | 0.14               | 0.08                                   | 43 ↓              |
| Zn        | 4.9                | 4.6                                    | 6↓                |

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(Braghiroli et al., 2019)



### N-rich residuals use in tailings revegetalization



Vb

#### Summary of main findings

#### N-rich zeolite

- <u>Plant biomasses</u> like tailings alone
- Foliar Na concentrations
  6-9 times higher than in other treatments



MBBR Biomass

- <u>Plant biomasses</u> like fertilized tailings and topsoil
- High Se concentrations in leaves

#### Better performance

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 Foliar N concentrations and <u>root biomasses</u> failed to discriminate between the two tested types of amendment

VS

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(Saint-Aimé et al., 2023)

## **Ongoing research**

#### Scientific knowledge for informed new practical applications

- **Organic cover**: is elevated water table required? Is water pumping through the cover necessary?
- Low-sulfides no-acid generating tailings cover: evolution and fate of potential contaminants under oxic vs anoxic and abiotic vs biotic conditions
- Passive NMD treatment in residual organics-based biofilters: contaminants removal mechanisms and residues stability\*
- Raw vs half-charred dolomite: prevention of AMD generation from pyrrhotite-rich tailings and passive polishing
- **N-rich residuals from mine water treatment**: potential of surrounding environment contamination (uptake by vegetation, runoff)





## **Concluding remarks**

- Successful rehabilitation approach for oxidized tailings on mine sites (precious and base metals) must combine prevention (tailings covering) and passive treatment
- **Residual materials valorization** (already available on or in the proximity) limits disposal concerns, environmental footprint, and mine sites rehabilitation costs
- Materials (natural and residual): efficient in mine tailings covers for AMD prevention or transformed, with promising results in contaminated mine water treatment
- Metal recovery, whenever feasible, could decrease water treatment costs
- Pilot scale production and testing of modified materials is limited
- Metal recovery, sorbent and treated water reuse, are rarely addressed



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## Thank you!



Merci!



### CCBE + passive treatment: Lorraine mine site



Free water

#### 1964-1968 : extraction of Cu, Au, Ag, Ni

acid-generating tailings: 15.5 ha (up to 6 m)



AMD: pH 3.6, 7 g/L Fe, 15 g/L sulfate

2000: CCBE + 3 dolomitic drains







#### Geochemical stability of Passive treatment system AMD Treated to be treated AMD PBR1 PBR2 In out in out in Out Sampling and environmental behavior evaluation Limits Stabilization/Solidification of post-treatment residues Post-treatment residues excavation s/s with GU s/s with GU/GGBFS s/s w Rain



AMD treatment solids

Leaching

# Plant material and growing conditions





<sup>1</sup>(Guittonny, 2021; Tordoff et al., 2000)

<sup>2</sup>(Guittonny, 2021)

<sup>3</sup>(Wiggans et Frey, 1955)



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