

# Passive treatment of highly contaminated iron-rich acid mine drainage

C.M. Neculita<sup>1</sup>, T.V. Rakotonimaro<sup>1</sup>, B. Bussière<sup>1</sup>,  
T. Genty<sup>1</sup>, G.J. Zagury<sup>2</sup>

<sup>1</sup> RIME, UQAT - University of Quebec in Abitibi-Temiscamingue

<sup>2</sup> RIME- Polytechnique Montréal, Department of Civil, Geological, and Mining Engineering

# Outline

- Context: Fe-rich AMD
  - Occurrence
  - Passive treatment
- Case studies
  - I) Lorraine mine site: lab vs field testing
  - II) East Sullivan mine site: 14 y water quality evolution
- Concluding remarks

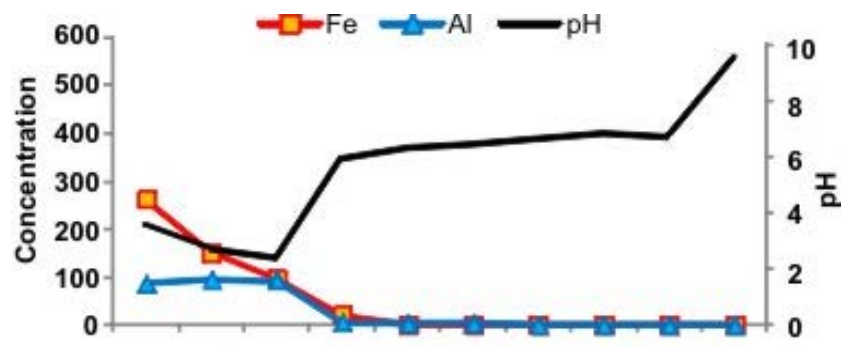
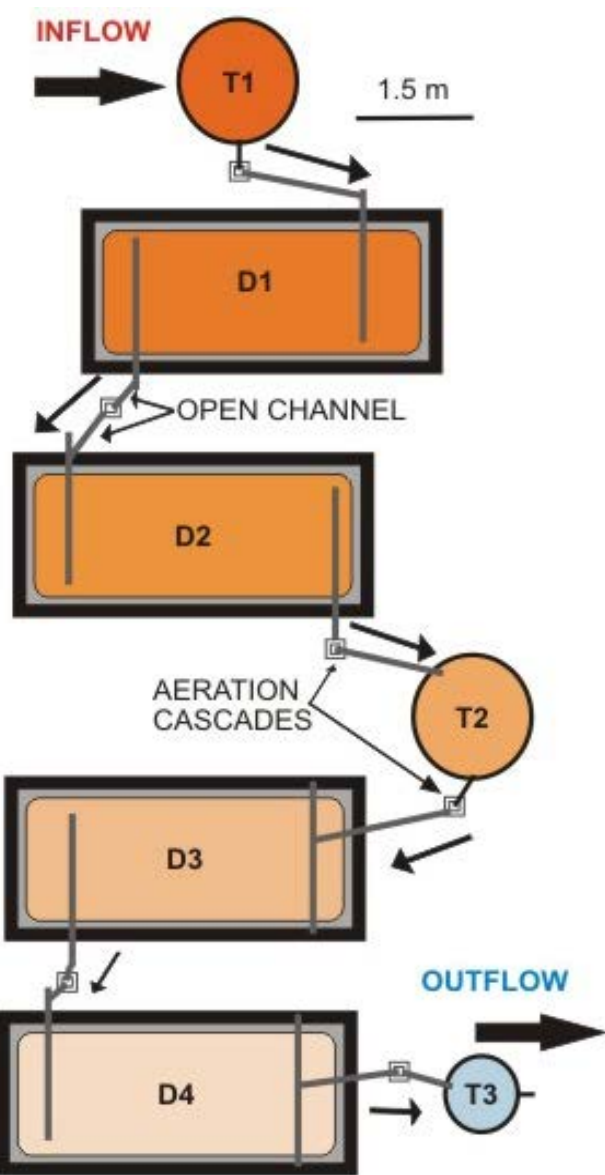
# Mine sites rehabilitation

- Step 1: Control AMD generation
  - Limit the availability of one (or more) of the three main contributing factors (sulfides, oxygen & water), or control tailings temperature
  - Example of developed methods
    - **Oxygen barriers (case study I and II)**
    - Water infiltration barriers
    - Desulphurization
    - Thermal barriers

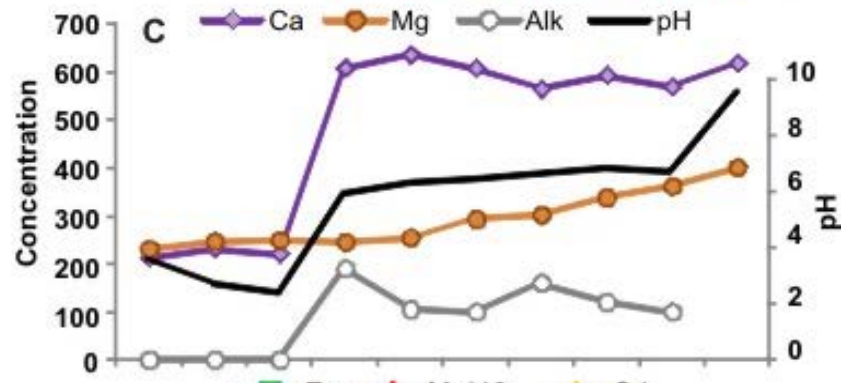
# Mine sites rehabilitation

- Step 2: Passive treatment of generated AMD
  - **Limestone/dolomite drains (DOL)**
    - pH and alkalinity increase, metals (and sulfate) precipitation
  - **Passive biochemical reactors (PBRs)**
    - Metals and sulfate removal
  - **Wetlands [(an)aerobic]**
    - Polishing of residual contaminants
  - **+ NEWER → Dispersed alkaline substrate (DAS) reactors:** mixtures of highly porous (wood chips) and alkaline (calcite, MgO) materials
    - Pre-treatment of high contamination loads

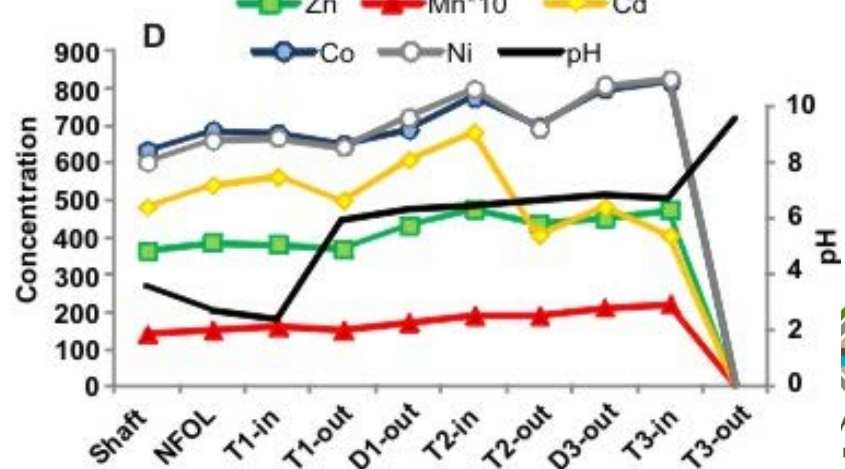
# Pilot-scale DAS reactors (T1-T3)



• T1 & T2: calcite-DAS



• T3: MgO-DAS



(Ayora et al., 2013)

# Examples of Fe-rich AMD

Comparison of **some of the most acidic waters and highest concentrations of metals** derived from tailings pore water, surface water, and underground mine workings (Moncur et al., 2005)

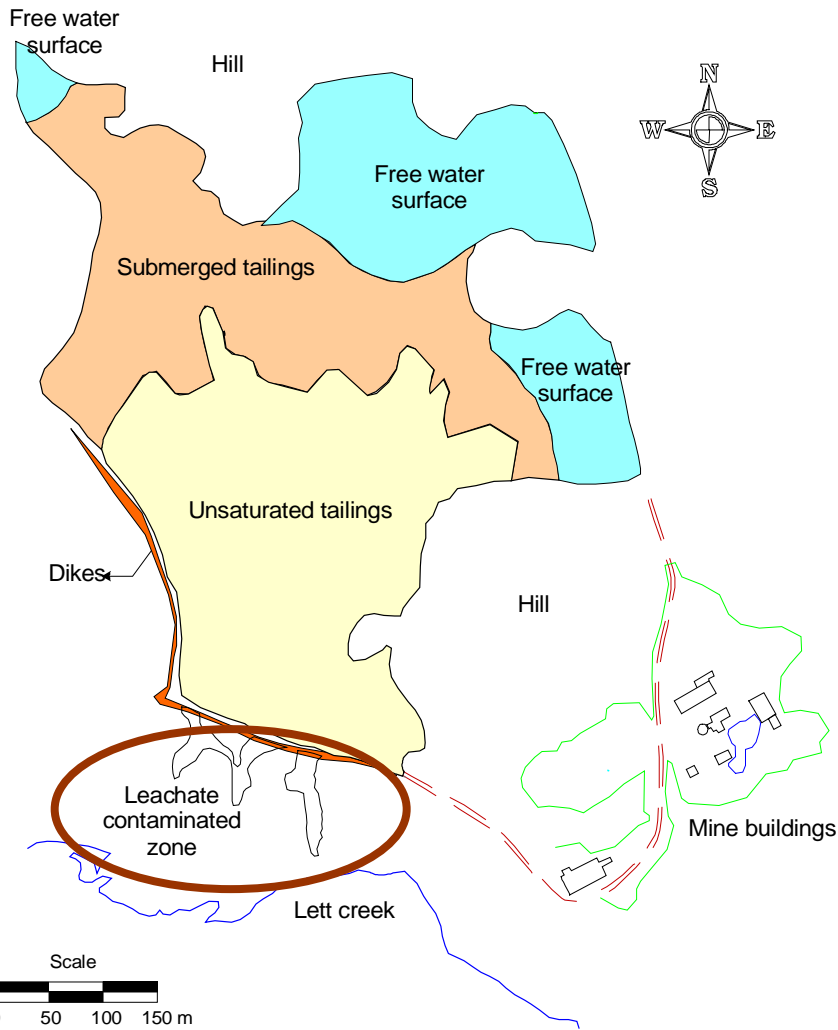
Parameter (g/L) (except pH)	pH	Cu	Zn	Cd	As	Fe <sub>t</sub>	SO <sub>4</sub> <sup>2-</sup>
Sheridan tailings (pore water), MB, Canada	0.67	1.6	55	0.1	0.05	129	280
Heath Steele (tailings pore water), NB, Canada	0.80	0.6	6	n/a	n/a	48	85
Genna Luas (surface water), Sardinia, Italy	0.60	0.22	10.8	0.06	0.07	77	203
Iron Mountain (mine shafts/drifts), CA, USA	-3.6	4.76	23.5	0.21	0.34	141	760
Other sites (mine shafts/drifts/pore water)	0.67	468	50	0.04	22	57	209

Parameter (g/L) (except pH)	pH	Cu	Zn	Cd	As	Fe <sub>t</sub>	SO <sub>4</sub> <sup>2-</sup>
Lorraine mine site, QC, Canada (Potvin, 2009)	3.6	n/a	0.8	0.4	n/a	6.9	15
East Sullivan mine site, QC, Canada (Germain et al., 1994)	2	n/a	n/a	n/a	n/a	7	17
*Carnoulès, France (Giloteaux et al., 2013)	1.2	n/a	n/a	n/a	12	20	29.6
Iberian Belt Pyrite, Spain (Macias et al., 2012)	3	0.005	0.44	n/a	n/a	0.3	3.6

# Case study I: Lorraine mine site

## - Historic, Progressive Rehabilitation

# 1 Lorraine mine site: historic



**1964-1968 : Cu, Au, Ag, Ni**  
**acid-generating tailings: 15.5 ha (up to 6 m)**



(Nastev & Aubertin, 2000)



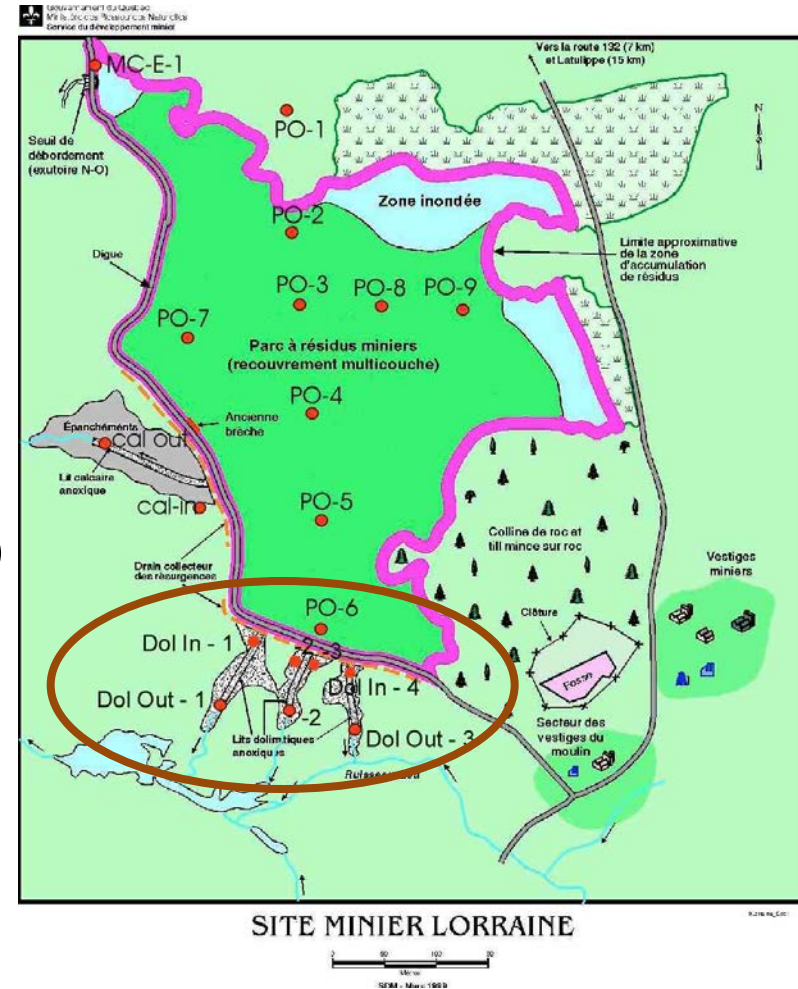
# 1 Lorraine mine site: rehabilitation

- **Control AMD generation**
  - Multilayer cover
- **Passive treatment of Fe-rich AMD**
  - Phase I: dolomite and calcite drains (1999) - chemical
  - Phase II: 3-unit system (2011) - biochemical
  - Phase III: DAS reactors (?) - biochemical
- **Passive treatment of Fe-rich AMD: challenges**
  - Limited space, topography, high water table
  - Abundant precipitation, harsh winter (7-8 months)
  - Lab testing required prior to construction of a field system

1

# Lorraine mine site: rehabilitation

- **1999: CCBE** (cover with capillary barrier effect = O<sub>2</sub> barrier): control AMD generation
- **1999: 3 Dolomite drains** (Dol-1 to Dol-3) and 1 calcite drain (Cal-1): passive treatment of Fe-rich AMD (Phase I)
  - pH 3.6, 7 g/L Fe, 15 g/L sulfate



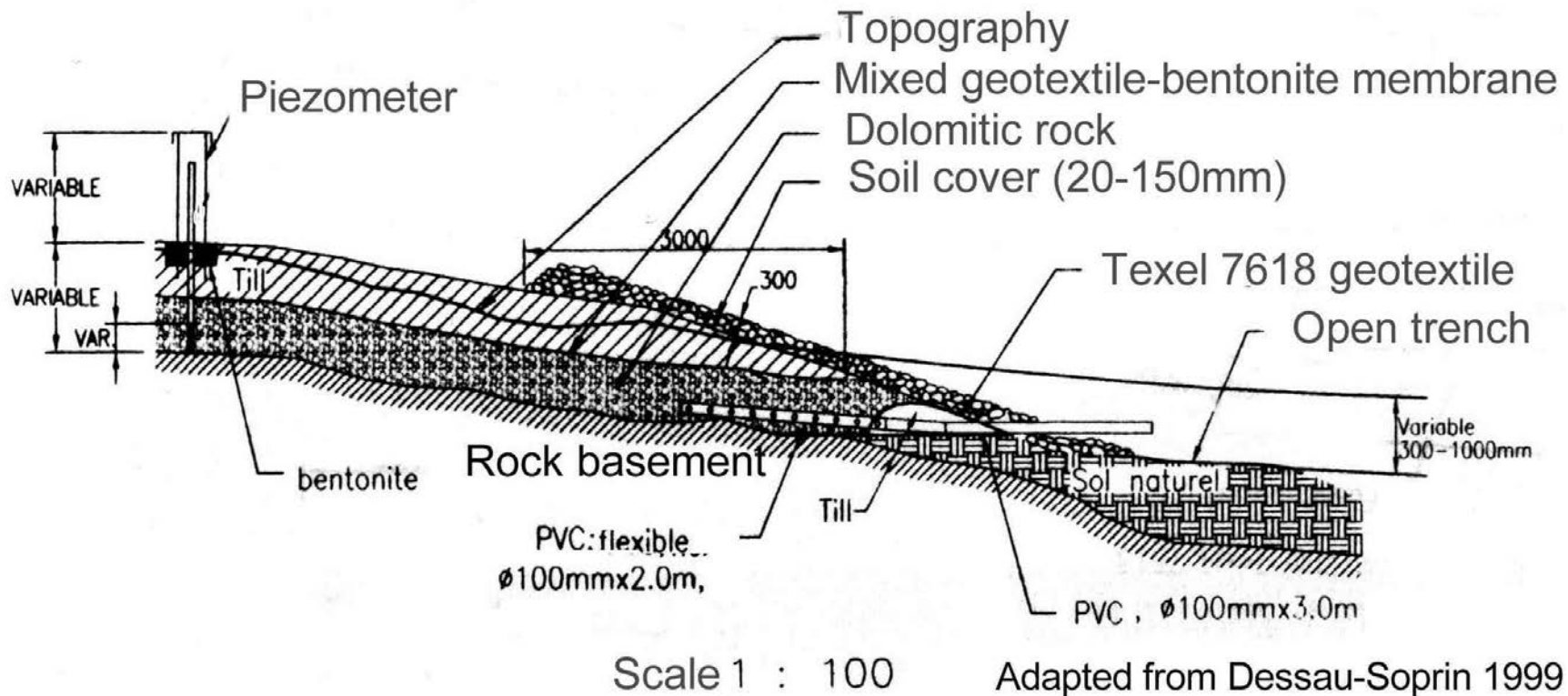
(Potvin, 2009)

# 1 Dolomite drains: design



Trenches filled with dolomite (70 %) (20-60mm)

- HRT (Dol-1 & Dol-2): 10 to 20 h



(Fontaine, 1999; Maqsoud et al., 2007)

# 1 Cal-1, Dol-1, and Dol-3

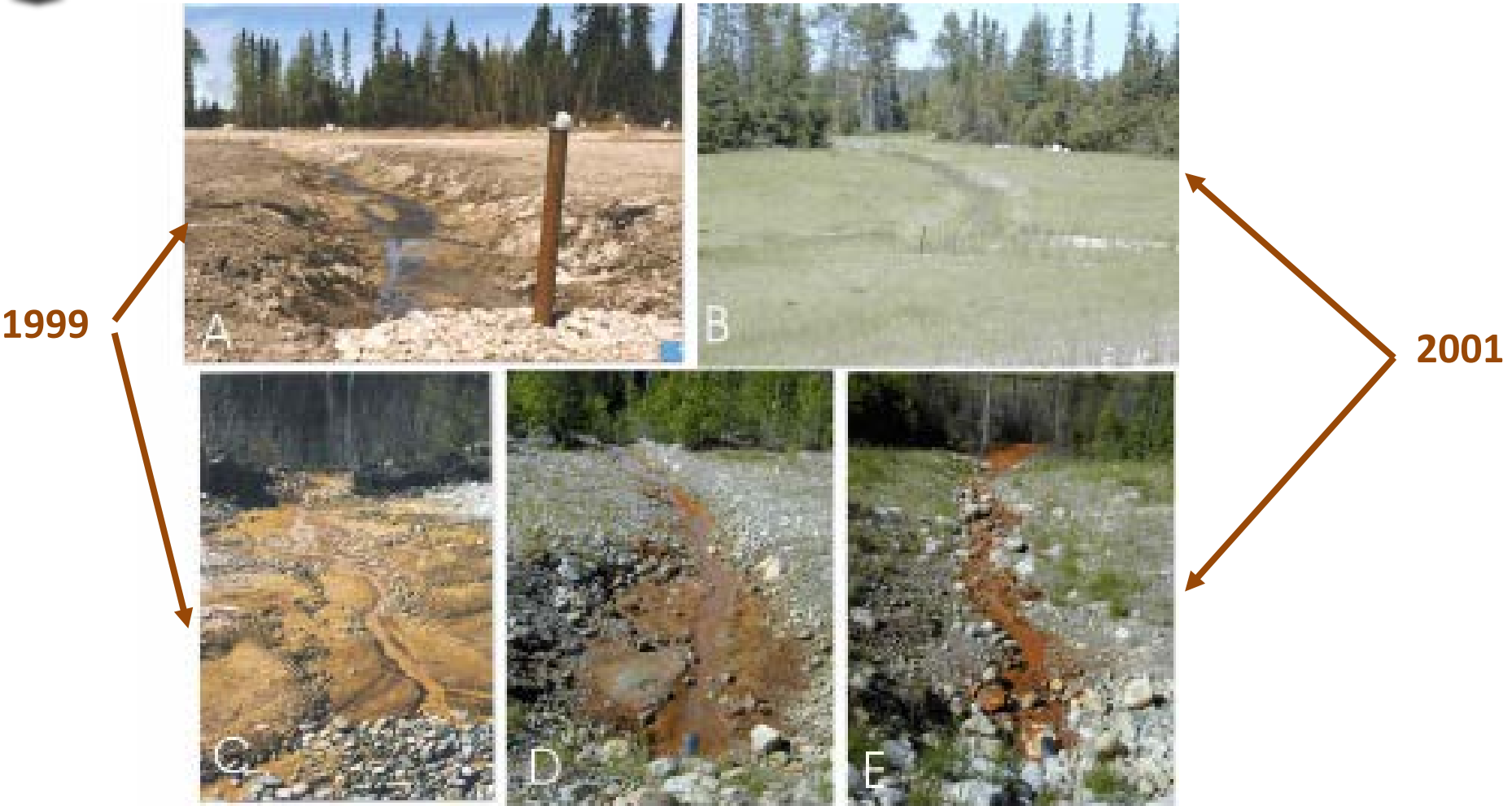


Figure 9 A) View of drain Cal-1 output, May 1999. B) Idem, but in June 2001. C) View of drain Dol-3 output, May 1999. D) Idem, but in June 2001. E) View of drain Dol-1 output, June 2001. Notice the iron hydroxides precipitates in the trenches.

(Bernier et al., 2002)

# 1 Dolomite/calcite drains: 1999-2001

**Tableau 3 Influent and effluent average pH, alkalinity and acidity.**

Sample	1999 (n=7)			2000 (n=6)		
	pH	Alkalinity	Acidity	pH	Alkalinity	Acidity
PO-6	3.17 (0.47)	0	5239 (341)	3.78 (0.36)	0	4525 (918)
Cal-1 out	6.72 (0.08)	470 (63)	0	6.82 (0.09)	468 (32)	0
Dol-1 out	6.09 (0.14)	145 (192)	116 (307)	6.19 (0.06)	88 (25)	0
Dol-2 out	5.37 (0.17)	8 (11)	2000 (1920)	5.57 (0.14)	4 (3)	0
Dol-3 out	4.44 (0.28)	0	2407 (1114)	4.70 (0.07)	0	3478 (878)

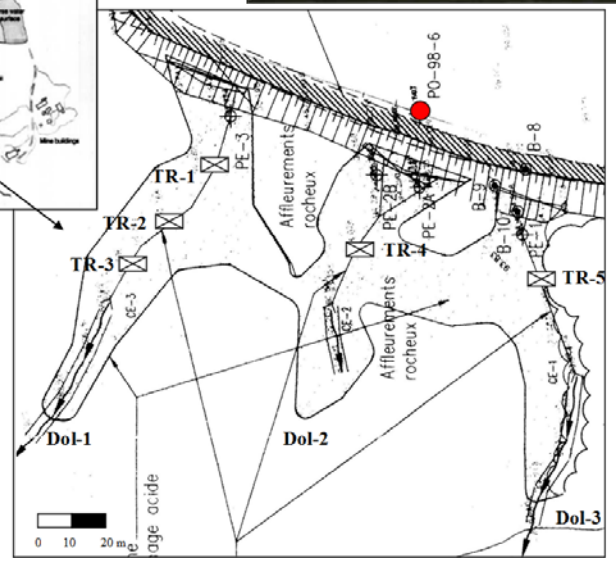
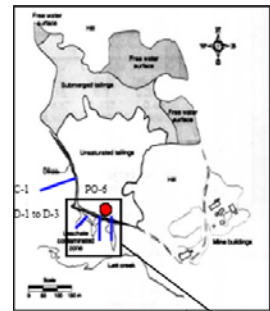
  

Sample	2001 (n=6)			2002 (n=4)		
	pH	Alkalinity	Acidity	pH	Alkalinity	Acidity
PO-6	3.81 (0.57)	0	6293 (1125)	4.16	0	8463 (382)
Cal-1 out	6.77 (0.06)	456 (47)	0	6.83 (0.08)	529 (61)	203 (26)
Dol-1 out	6.14 (0.08)	58 (31)	0	6.18 (0.1)	110 (70)	1076 (36)
Dol-2 out	5.64 (0.08)	4 (6)	3160 (1614)	5.49 (0.07)	5 (10)	4865 (124)
Dol-3 out	4.74 (0.16)	0	3432 (986)	4.4 (0.08)	0	4760 (576)

*Alkalinity and acidity are in mg CaCO<sub>3</sub>/L*

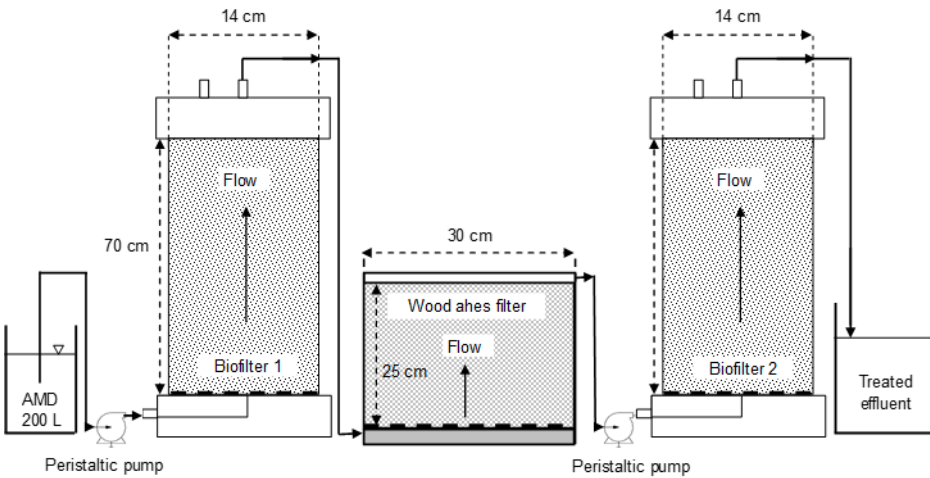
(Bernier et al., 2002)

# 1 Dol-3 (2009): clogged



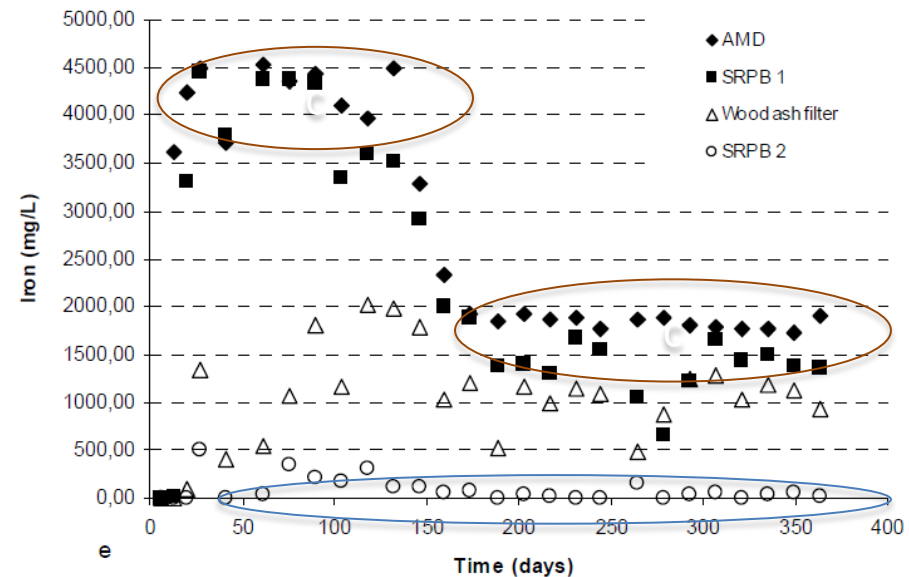
(Potvin, 2009)

# 1 Phase II: lab testing (6.7L to 2m<sup>3</sup>)



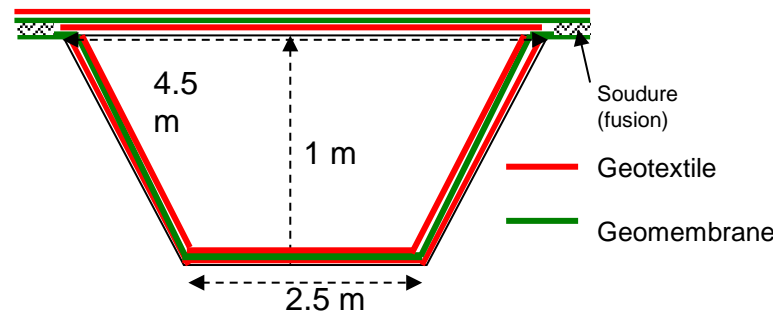
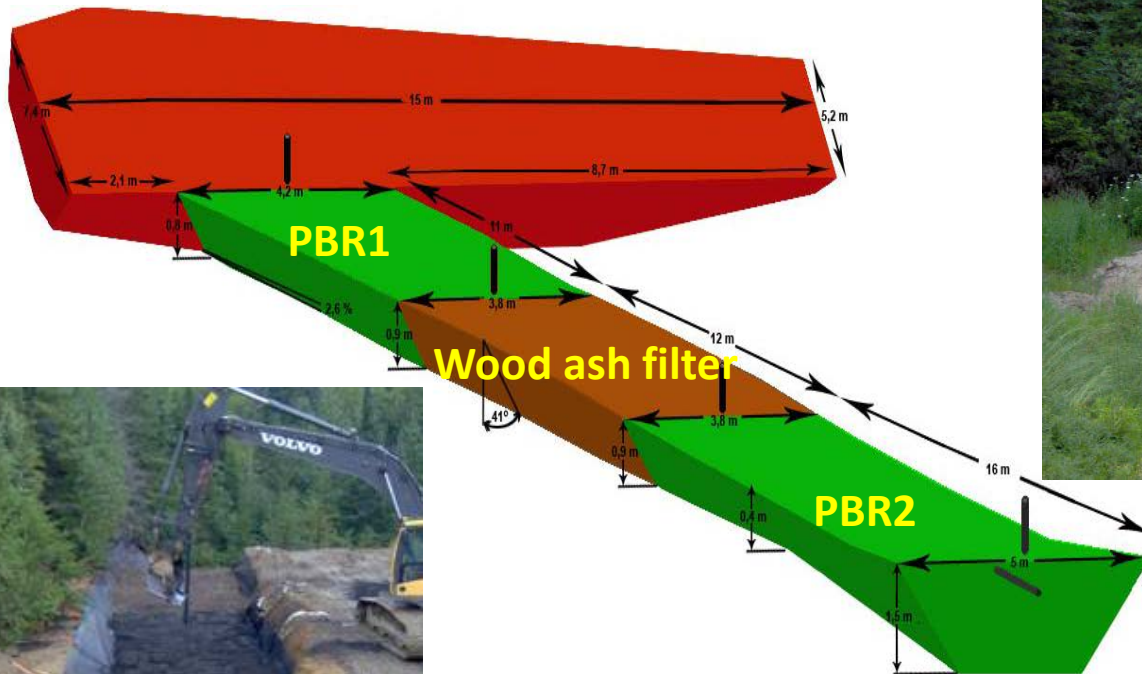
## 3-unit train lab system

- Input Fe: 2-4 g/L
- Output Fe: < 1 mg/L



(Genty, 2012)

# 1 Field pilot construction: design



Components (% dw)	PBR1	PBR2
Wood chips	36	18
Manure	17	10
Compost	24	12
Sand	21	10
Calcite	2	50

(Genty, 2012)



# 1 Field pilot construction: within 5 days



Before Dol-3 excavation



Dol-3 excavation



Material mixing



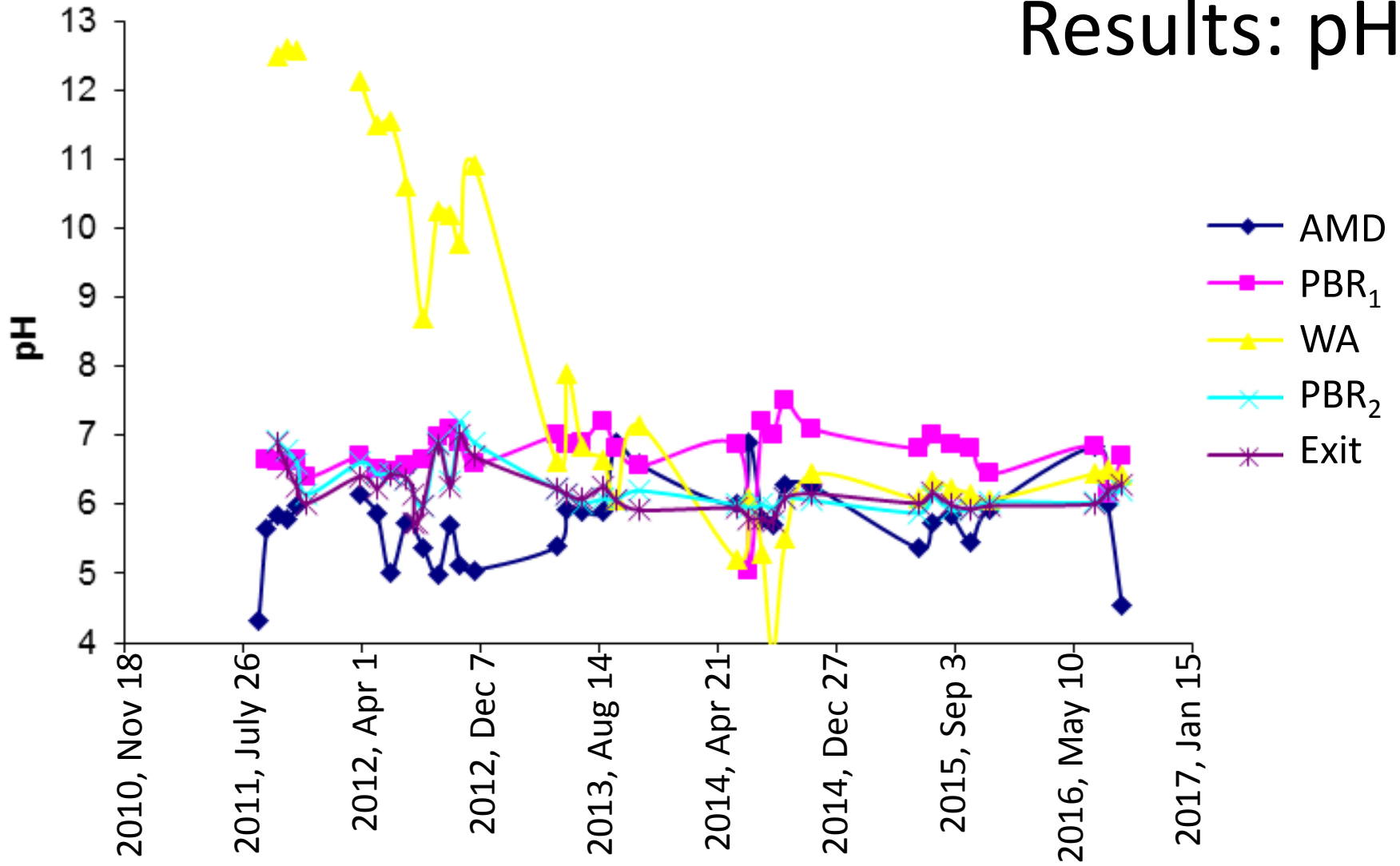
AMD drain collection

**PRIME**  
TECHNIQUE

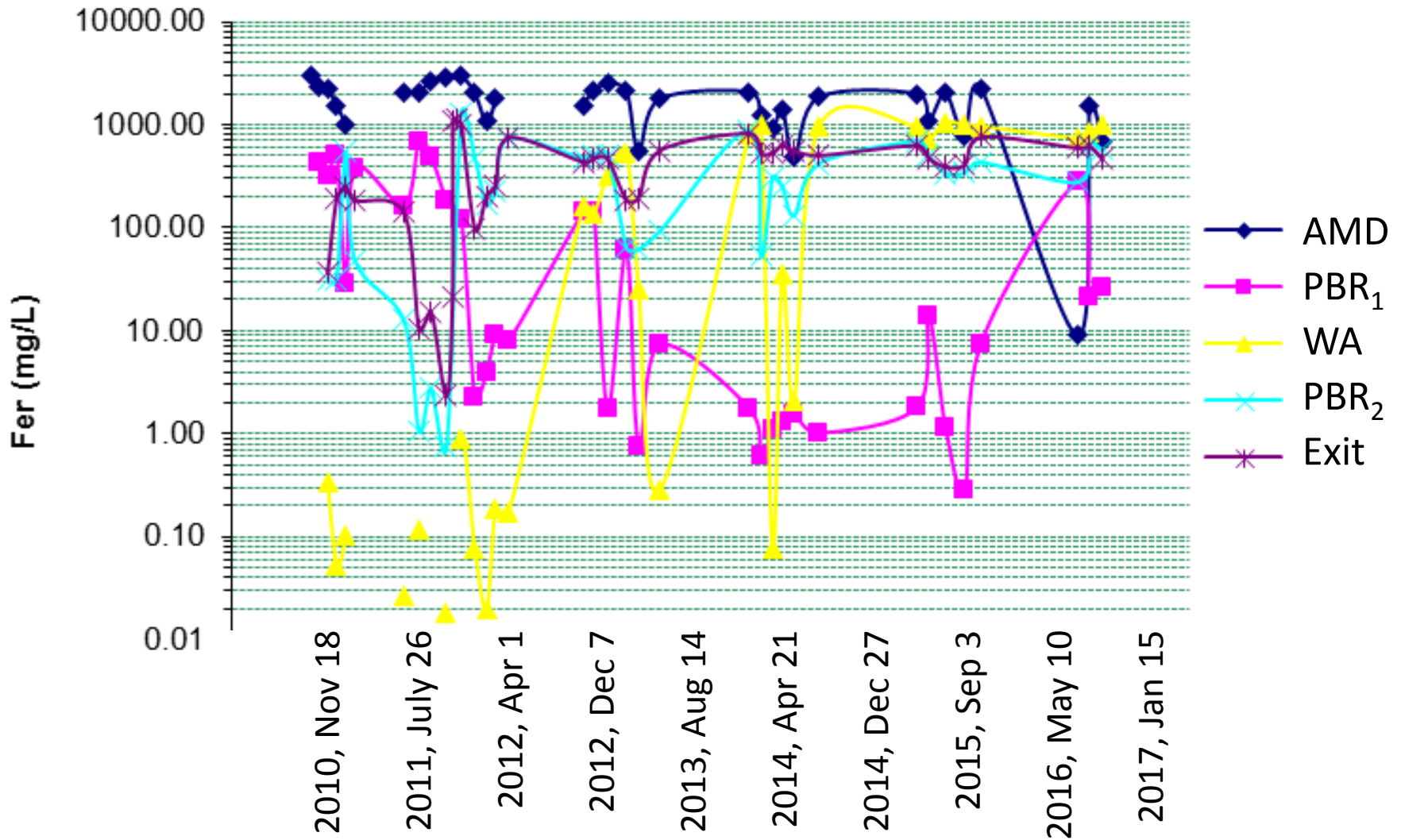
# 1 Field pilot construction: within 5 days



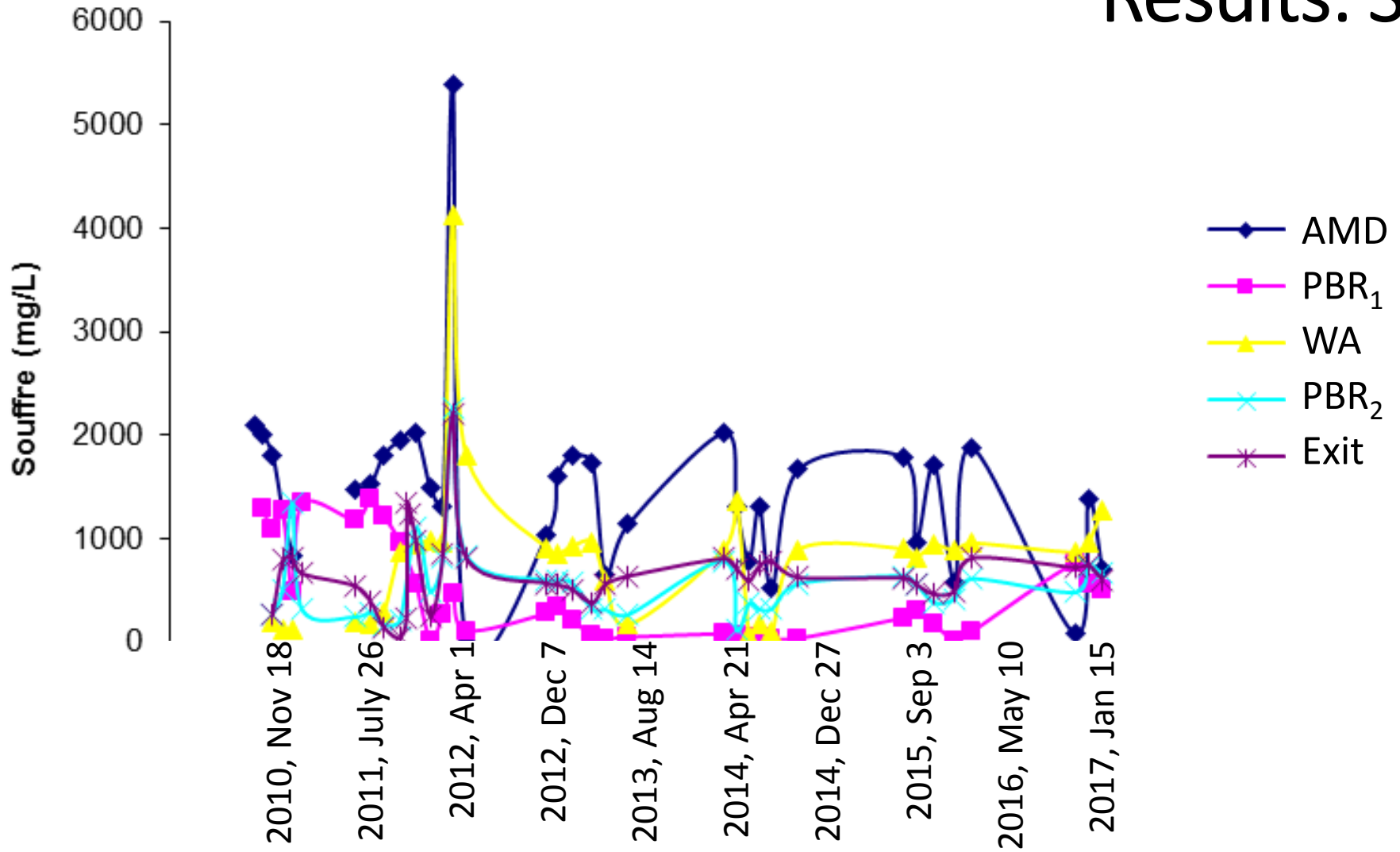
# Results: pH



# Results: Fe



# Results: S



# 1 Monitoring data (2011-2016)



- Metals / metalloids removal
  - Compliance with regulation, except for Fe (and Mn)

Characteristics	pH	As	Cu	Fe	Ni	Pb	Zn
		(mg/L)					
AMD	4.3 – 6.9	<0.06	<0.003	1 800	0.62	0.19	0.26
Treated effluent	5.8 – 7	<0.01	<0.003	411	0.06	0.03	0.07
Best quality (August 2015)	6	<0.01	<0.01	389	<0.004	<0.07	0.06
<b>Quebec discharge regulation</b>	<b>6-9</b>	<b>0.2</b>	<b>0.3</b>	<b>3</b>	<b>0.5</b>	<b>0.2</b>	<b>0.5</b>
<b>Compliance with regulation</b>	<b>YES</b>	<b>YES</b>	<b>YES</b>	<b>NO</b>	<b>YES</b>	<b>YES</b>	<b>YES</b>

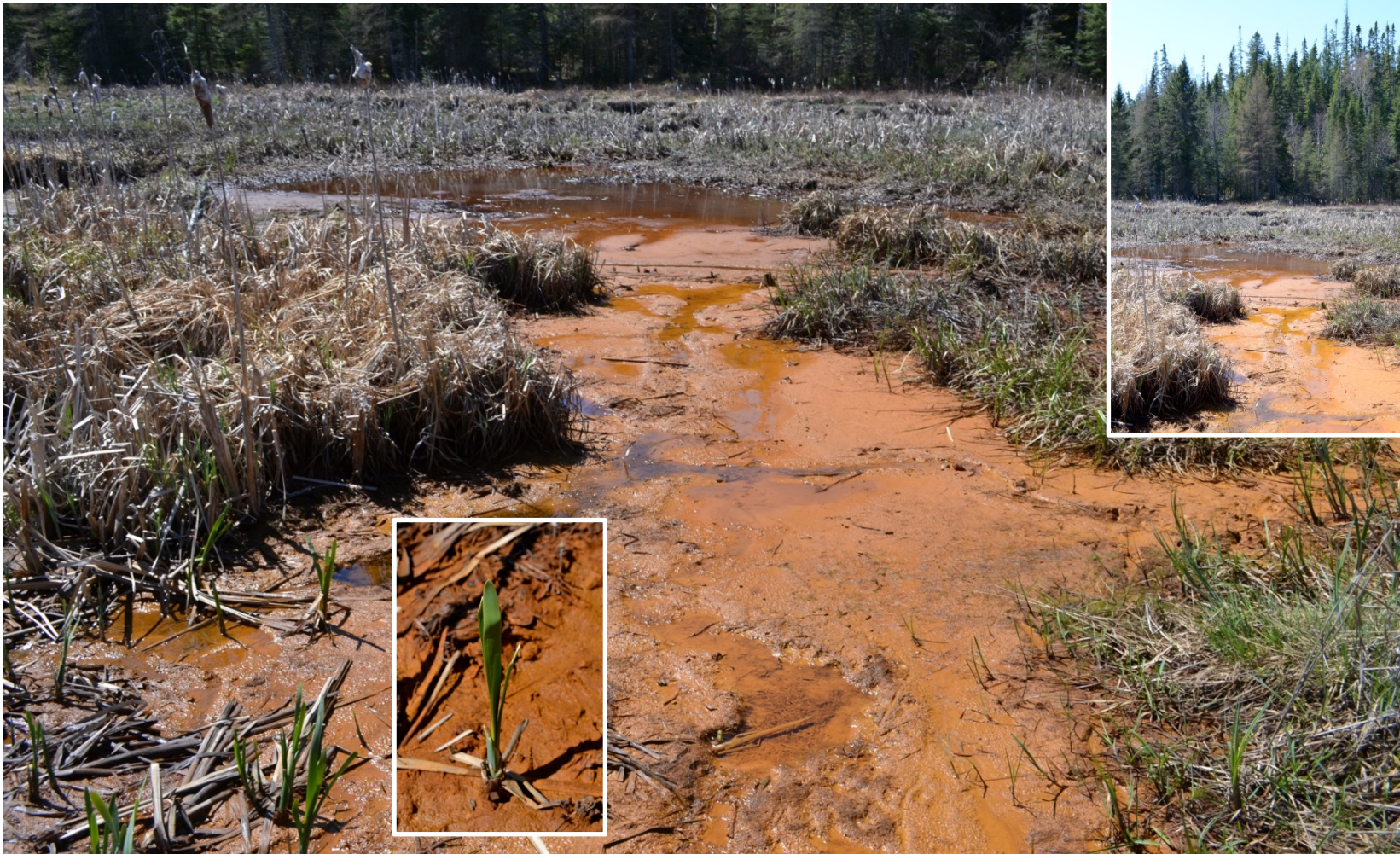
(Genty et al., 2016)

# 1 Cascade aeration downstream (2016)



(Rakotonimaro, 2017)

# 1 Natural wetland downstream (2016)



(Rakotonimaro, 2017)



# 1 Dolomite drains: 2016

Dol-1



Dol-2

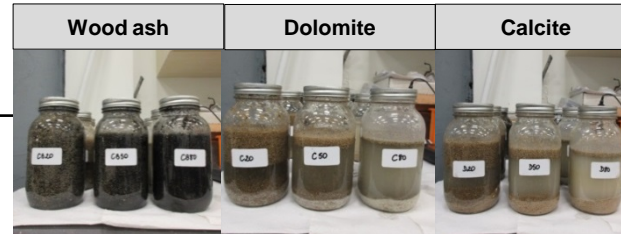


(Rakotonimaro, 2017)

# 1 Phase III: lab testing (2 years)

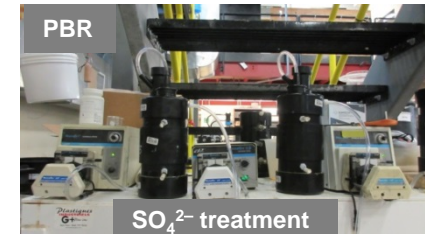
## Step 1 – Batch testing (1 L)

Selection the most efficient DAS



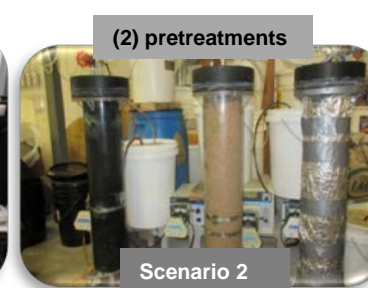
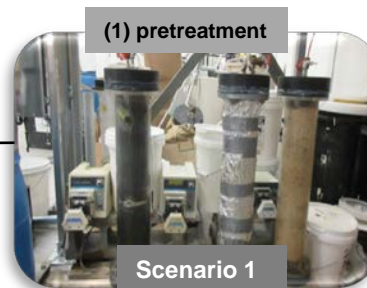
## Step 2 – Column testing (1,7 L)

Select optimal HRT (1–5 d);  
Evaluate  $k_{sat}$  and  $n$



## Step 3 – Multi-step (10,7 L)

Performance evolution



**Synthetic AMD: pH 4, 2.5 g/L Fe, 5.4 g/L  $SO_4^{2-}$**

**Monitored parameters: physicochemical, hydraulic, microbiological, mineralogical**

HRT: Hydraulic Retention Time;  $k_{sat}$ : permeability;  $n$ : porosity

# 1 Results: batch testing

## DAS reactors and PBRs

- Most efficient mixture: DAS-wood ash
  - High pH (6.25 - 7.14) and alkalinity
  - 4 h of contact time enough, if Fe < 1.5 g/L
  - 6–11h required, if Fe initial > 1.5 mg/L
  - WA50 (50% wood ash, 50 % wood chips): optimal
- DAS- calcite and DAS-dolomite: comparable efficiency
  - DAS- calcite : more efficient than DAS-dolomite, only temporarily
  - C20 (20% calcite, 80% wood chips): used as post-treatment
- Low SO<sub>4</sub><sup>2-</sup> removal in all reactors

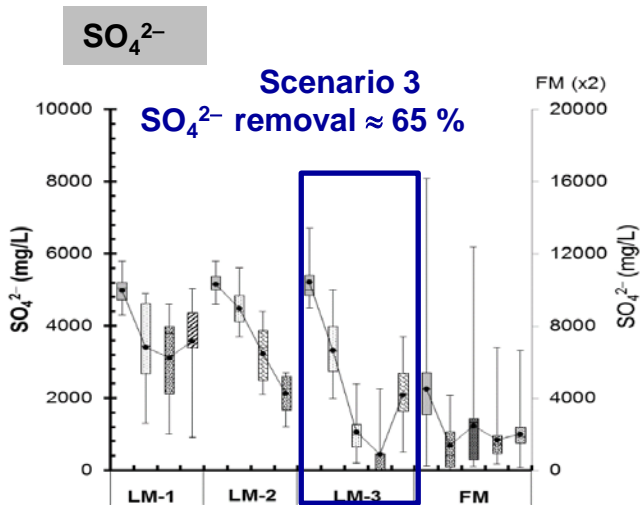
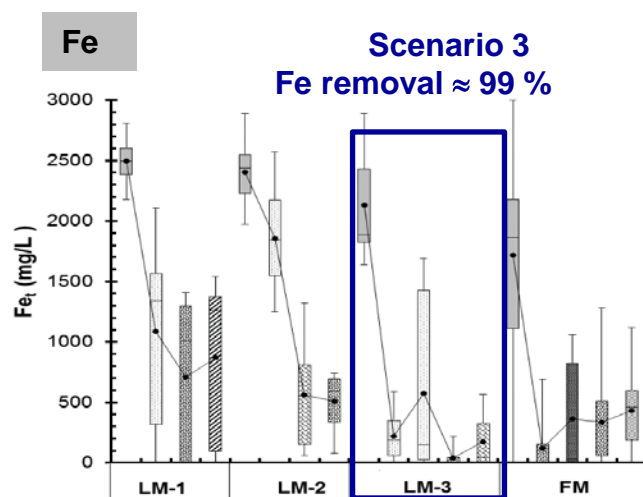
# 1 Results: column testing

Parameters	DAS reactors		PBRs	
	WA50	C20	2.5d HRT (R2.5)	5d HRT (R5)
pH	5.3–6.3	6–7	6.2 ± 0.5	6.6 ± 0.5
Alkalinity (mg CaCO <sub>3</sub> /L)	130–350	16–50	90–2300	430–2800
Acid neutralisation (%)	62	18–47	66	76
Fe removal (%)	up to >96	47–73	77	91
SO <sub>4</sub> <sup>2-</sup> removal (%)	<35	<5	<5	13

- WA50, R5: maximal efficiency at 5d of HRT
- C20: maximal efficiency at 2d of HRT, temporarily
- Low SO<sub>4</sub><sup>2-</sup> removal in PBRs

# 1 Comparative performance: lab vs. field

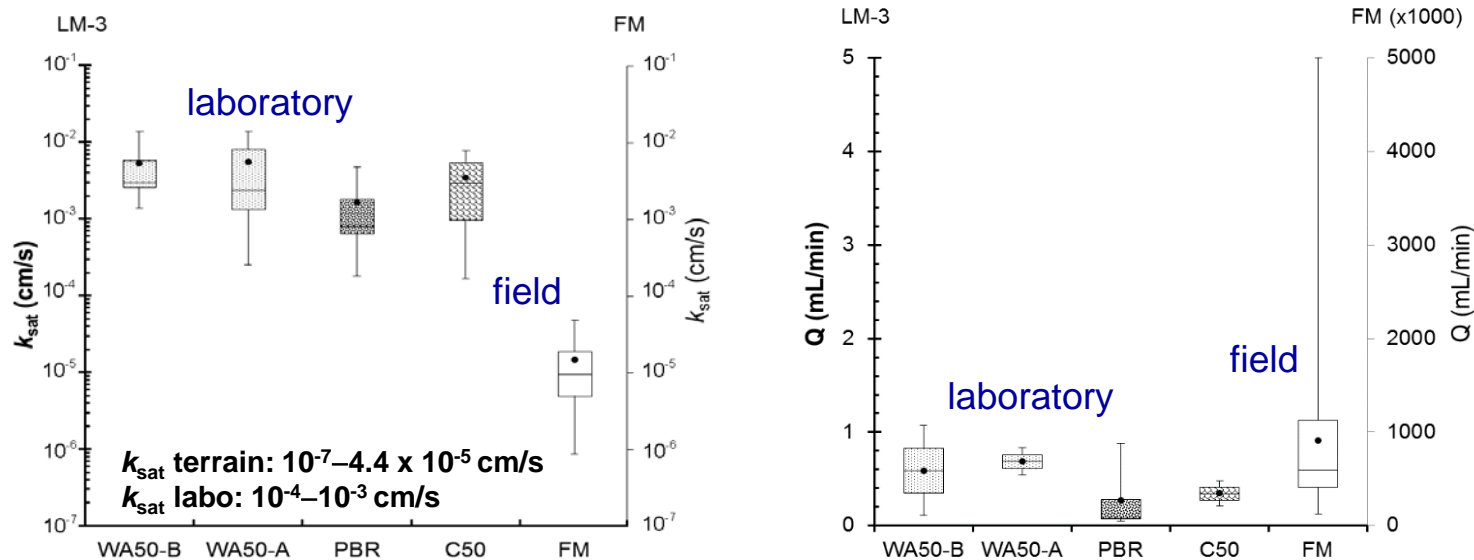
- **Multi-step** – Laboratory vs field (Fe and  $\text{SO}_4^{2-}$  removal)



- Lab: **best efficiency with scenario 3**
- Field: **91 % Fe** (first 2 years), then 53 %  
**68 %  $\text{SO}_4^{2-}$**  (first 2 years), then 43 %

# 1 Comparative results: lab vs. field

- **Multi-step** – Laboratory vs field (hydraulic evolution)



- $k_{sat}$  labo = 1–2 order of magnitude higher than  $k_{sat}$  terrain
- Q variable in field (HRT = variable)  $\neq$  Q lab controlled (HRT = ct)

# 1 Comparative results: literature

System type	Design factors	References
<b>Biochemical</b>		
Anaerobic wetland (AnW)	3,5 g acidity/m <sup>2</sup> /d ; 10 g Fe/m <sup>2</sup> /d	Hedin et al (1994); Skousen and Ziemkiewicz (2005)
Vertical flow wetland (VFW)	35 g acidity/m <sup>2</sup> /d	Kepler and McCleary (1997)
PBR (mussel shell) (initial Fe = 65,8 mg/L SO <sub>4</sub> <sup>2-</sup> = 608 mg/L)	29 g SO <sub>4</sub> <sup>2-</sup> /m <sup>3</sup> substrate/d (94%)	McCauley et al (2009)
<b>PBR (calcite)</b> (Following two DAS; initial Fe ≈ 35 mg/L; SO <sub>4</sub> <sup>2-</sup> ≈ 1000 mg/L)	<b>4–73 g Fe/m<sup>3</sup>/d, 2–117 g SO<sub>4</sub><sup>2-</sup>/m<sup>3</sup>/d (≈ 99 %)</b>	<b>Rakotonimaro (2017)</b>
<hr style="border-top: 1px dashed black;"/>		
<b>Geochemical</b>		
Anoxic limestone drain (ALD)	15 h residence time; 50 g acidity/t/d	Watzlaf (2004); Skousen and Ziemkiewicz (2005)
Limestone leach bed (LLB)	2 h residence time ; 10 g acidity/t/d	Skousen and Ziemkiewicz (2005)
DAS (C20) (initial Fe = 250 mg/L)	HRT (1 d), 42 % Fe	Rötting et al (2008a)
<b>DAS (C20)</b> (initial Fe ≈ 2000 mg/L)	<b>Fe (73%, HRT = 2 d)</b>	
<b>DAS (C50)- pretreatment</b> (initial Fe = 1800 mg/L)	<b>Fe (67%, HRT = 3 d)</b>	<b>Rakotonimaro (2017)</b>
<b>DAS (WA50)</b> (initial Fe ≈ 2000 mg/L)	<b>Fe (&gt; 89% , HRT = 3 d)</b>	

(Skousen et al., 2017; Rakotonimaro, 2017)

# 1 Summary

- DAS-wood ash: most efficient for Fe pre-treatment
- 2 units of pre-treatment : more efficient than one
- DAS-calcite and DAS-dolomite: comparable efficiency
- No clogging issues in lab testing
- Treatment performance (lab / field) depends on Q, Fe,  $\text{SO}_4^{2-}$

## Future work

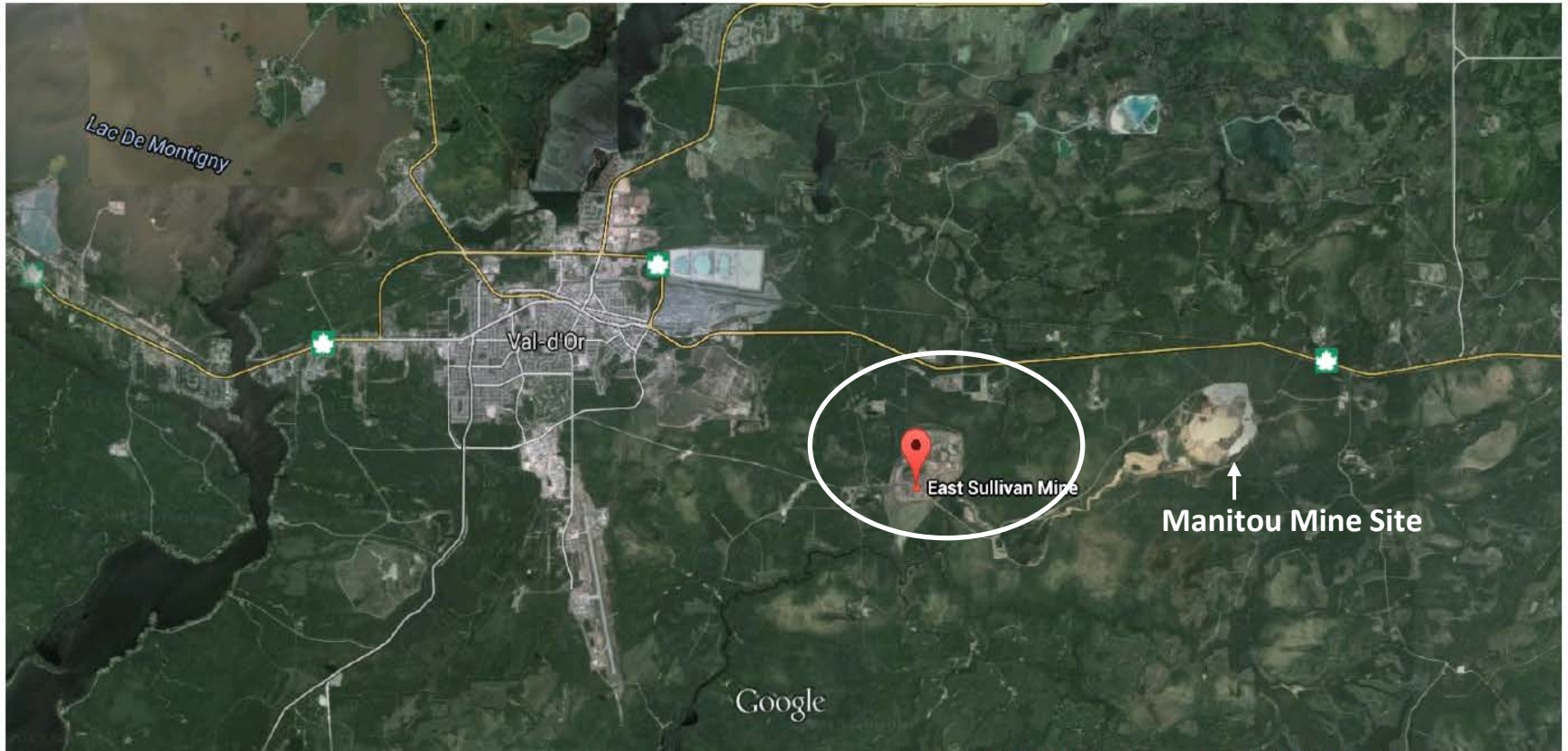
- Excavation of the 3 units and replacement by 2-3 DAS systems
- Mineralogical and microbiological characterization of solids



# Case study II: East Sullivan mine site

## - Historic, Rehabilitation

## 2 Location



Imagery ©2015 DigitalGlobe, Cnes/Spot Image, Map data ©2015 Google 2 km

6 km E of the Val-d'Or town, SW QC, Canada

## 2 East Sullivan mine site: historic

1945



1990



**1942-1979 : Cu, Zn, Au, Ag, Cd**

- **15 Mt (200 ha) of tailings, 200kt of acid generating material; 228 ha impacted**
- **3.6% S, thickness of 7.3 m in average**

<http://sebastienlavoie.com/maitrise/photos.html>

<http://www.mrn.gouv.qc.ca/mines/restauration/restauration-sites-east-sullivan.jsp>

# 2 East Sullivan mine site

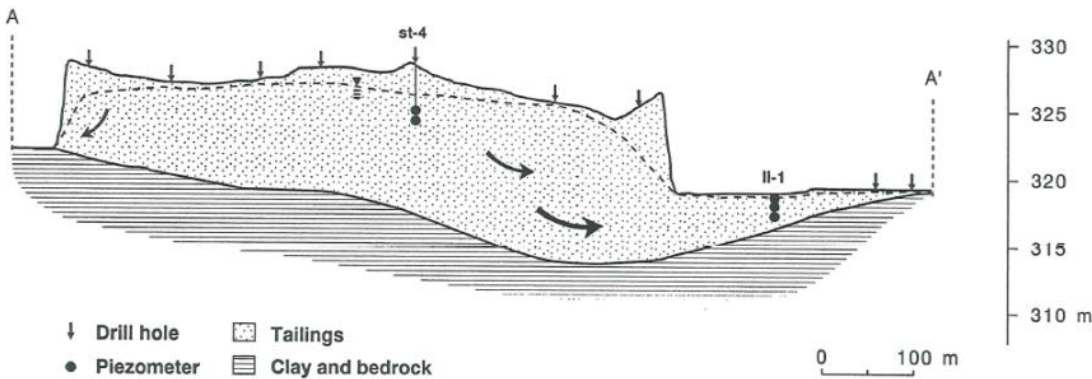


Figure 2. Cross-section A-A' through the East-Sullivan tailings impoundment. Arrows indicate locations of drill holes to the bedrock or clay basement. Dots represent piezometer locations for water sampling.

## ○ Pore-water quality in 1990

- pH  $\approx$  2
- Fe ( $\text{Fe}^{2+}$ ): up to 17 g/L
- $\text{SO}_4^{2-}$ : up to 37 g/L
- Cu, Pb, Zn : 0.1-1 g/L

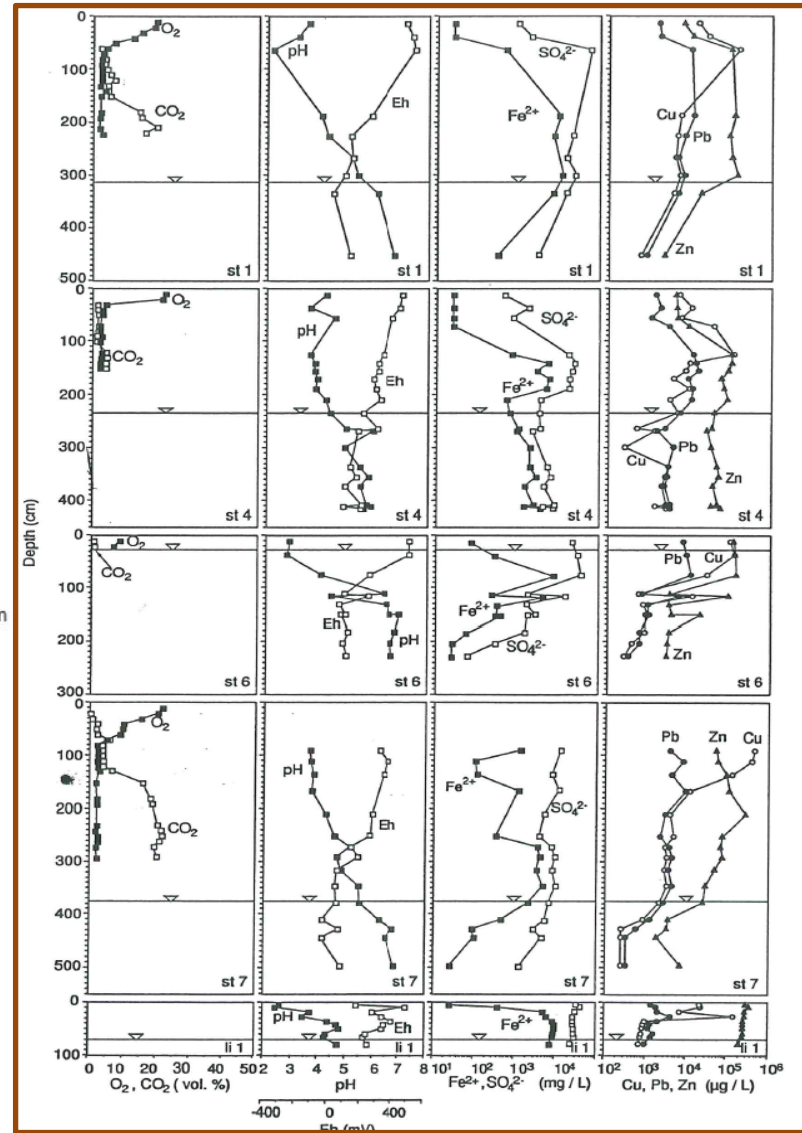


Figure 3. Profiles of  $\text{O}_2$  and  $\text{CO}_2$  in pore gases and of pH, Eh,  $\text{Fe}^{2+}$ ,  $\text{SO}_4^{2-}$ , Cu, Pb, and Zn in pore-waters at the five selected stations located in Figure 1. The line with the triangle indicates the average water-table depth during the sampling period.

(Germain et al., 1994)

## 2 East Sullivan: rehabilitation

- **1984: Wood waste cover (prevention and treatment)**
- **1990: Seepage collection system**
- **1992-1996: Confining dike (6 km)**
- **1998-2005: “Active” treatment of collected AMD in wetlands**
- **[2014: Wood cover of the eastern sector, not completed]**

⇒ **Some effluents are still acidic**

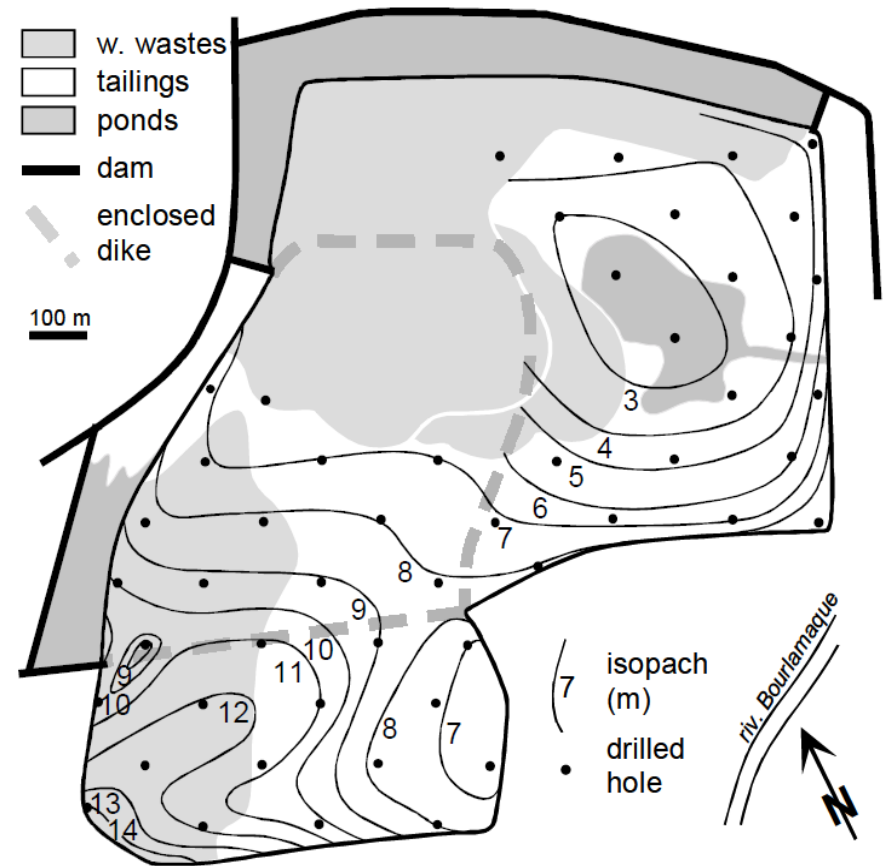
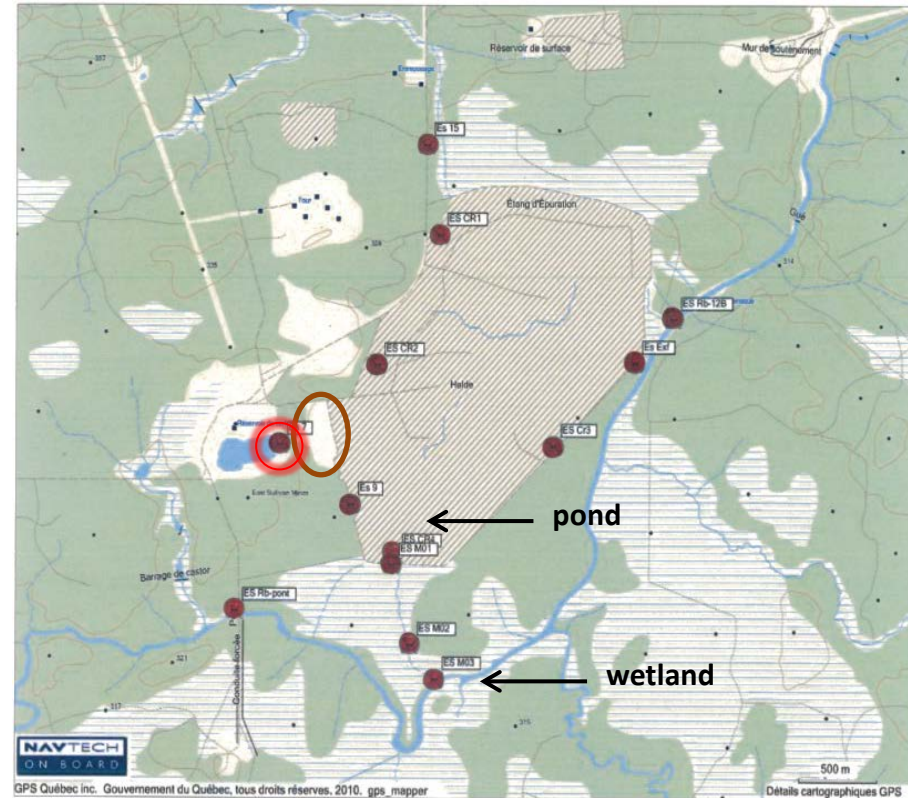


Figure 1. Map of the East Sullivan tailings impoundment in 1994

## 2 East Sullivan: monitoring (2000-2014)

- 12 sampling points
  - 7 points: dam and settling ponds
  - 5 points: tailings edges
- Parameters
  - pH, alkalinity, TDS, Fe, Al, Mn, Cu, Zn, Pb,  $\text{SO}_4^{2-}$
- Compliance, except for the uncovered tailings area



## 2 Summary

- Efficiency of wood-waste cover for over 14 years
- Significant improvement of water quality
- Site presently turning into birds' refuge (southern and eastern ponds, more than 190 species listed)

### Future work

- Completion of the eastern part of tailings by wood-waste and sludge (< 10% of total)
- Mineralogical / microbiological characterization of solids
- Further risk assessment

# 2 East Sullivan: 2015



Eastern pond



Eastern tailings



(Rakotonimaro et al., 2015)



# Concluding remarks

- Use of residual materials (dolomite, wood ash, compost, manure): low cost
- Relatively easy to install and operate
- Maintenance (more or less) required

BUT

- Limited performance at high contamination level:  
**multi-step systems (?)**
- Unpredictable long-term efficiency
- Solutions not available for sludge management

**However, sometimes is the only available option**



# References

- Ayora, C., Caraballo, M.A., Macías, F., Rötting, T.S., Carrera, J., Nieto, J.-M., 2013. Acid mine drainage in the Iberian Pyrite Belt: 2. Lessons learned from recent passive remediation experiences, *Environ. Sci. Pollut. R.* 20: 7837-7853.
- Caraballo, M.A., Maciàs F., Rötting, T.S., Nieto, M.J., Ayora, C., 2011. Long term remediation of highly acid mine drainage: a sustainable approach to restore the environmental quality of the Odiel river basin. *Env. Pollut.* 59: 3613-3619.
- Environmental Protection Agency USA (USEPA), 2017. Industrial effluent guidelines. <https://www.epa.gov/eg/industrial-effluent-guidelines> (access March 2017).
- Genty, T., 2012. Comportement hydro-bio-géochimique des systèmes passifs de traitement du drainage minier acide fortement contaminé en fer. PhD dissertation. Sci. Appl., UQAT, Rouyn-Noranda, QC, Canada. 248 p.
- Hamilton, Q.U.I., Lamb, H.M., Hallett, C., Proctor, J.A., 1999. Passive treatment for the remediation of acid mine drainage at Wheal Jane, Cornwall. *J Water Environ.* 13 (2): 93-103.
- Ministère du Développement durable Environnement et Lutte contre les Changement Climatiques (MDDELCC), 2012. Directive 019 sur l'industrie minière. Gouvernement du Québec. 105p.
- Neal, C., Whitehead, P.G., Jeffery, H., Neal, M. 2005. The water quality of the River Carnon, West Cornwall, November 1992 to March 1994: the impacts of Wheal Jane discharges. *Sci. Total. Environ.* 338: 23-39.
- Skousen, J., Zipper, C.E., Rose, A., Ziemkiewicz, P.F., Nairn, R., McDonald, L.M., Kleinmann, R.L., 2017. Review of passive systems for acid mine drainage treatment. *Mine Water Environ.* 36 (1): 133-153.
- Rakotonimaro, T.V., 2017. Pretreatment and passive treatment of Fe-rich acid mine drainage. PhD dissertation. UQAT, Canada. 250 p.



**A UNIQUE RESEARCH  
PROGRAM** in Québec

